



BETO 2021 Peer Review: Enhancing Acetogen Formate Utilization to Value-Added Products 2.3.2.112

Jonathan Lo National Renewable Energy Laboratory Conversion March 11, 2021

This presentation does not contain any proprietary, confidential, or otherwise restricted information

Market Trends

Product

Feedstock

Capital

Anticipated decrease in gasoline/ethanol demand; diesel demand steady
(Increasing demand for aviation and marine fuel
Increasing demand for renewable/recyclable materials
Decreasing cost of renewable electricity
Sustainable waste management
Expanding availability of green H ₂
Olosing the carbon cycle
Challenges and costs of biorefinery start-up
Carbon intensity reduction

NREL's Bioenergy Program Is Enabling a Sustainable Energy Future by Responding to Key Market Needs

Value Proposition

- How do we utilize CO₂ with cheaper renewable energy?
- What products can we make?

Differentiator

- Liquid C1 compounds as medium for microbial upgrading
- Diversity of potential inputs
- Long term temporal storage, easy transport

Quad Chart Overview

Timeline

• 10/01/2018 through 9/30/2021

	FY20	Active Project
DOE	(10/01/2018 –	\$850,000 for 3
Funding	9/30/2021)	years

Barriers addressed

Ct-H – C1 Fermentation Development

Liquid C1s are a novel and promising avenue for microbial conversion to bioproducts, but little is known about C1 liquid fermentation processes

Ct-D – Advanced Bioprocess Development Liquid C1s can be derived from a variety of renewable feedstocks and utilized in a variety of ways, but no industrial process exists

Project Goal

- Develop acetogens as a platform for renewable liquid C1 conversion to value-added products
- Perform TEA/LCA analysis to understand CO₂ and economic considerations

End of Project Milestone

- Demonstrate production of 2 g/L of C4 compound C1 feedstocks
- TEA/LCA analysis of potential process with generated fermentation metrics

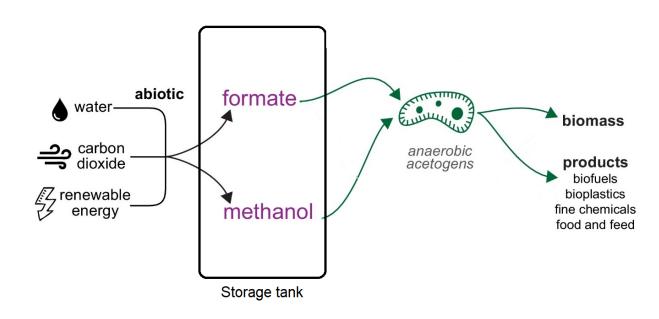
Funding Mechanism

Funded through BETO Conversion 2018 Lab call

Project Overview

- Liquid C1 compounds represent an understudied avenue for renewable energy capture and CO₂ bioconversion
 - Electro/thermochemical approaches have focused on syngas (H₂, CO)
 - CO₂ capture to liquid feedstock (methanol/formate)
 - <u>High energy density</u> Formate = 53 g/L H_{2} , methanol = 100g/L H_{2}
 - <u>Easily stored/transported</u>
 - <u>Miscible</u> Avoiding mass transfer limits

- **Goal**: Develop a biological approach to convert liquid C1 into products
- Combine renewable chemical CO₂ reduction with biological upgrading



Renewable energy conversion of CO₂ combined with biological upgrading Adapted from Cotton et al. 2020 j.copbio.2019.10.002

Project Overview

- **Relevance**: Chemicals with CO₂ and low-cost energy as feedstocks
 - Low-cost electricity to chemically reduce CO2 to formate/methanol
 - Scalable strategy as a stand-alone process or value add to existing industry
- Outcomes:

– Proof of concept:

- General process outline
- Feedstocks and Organism Identification/Characterization
- Soluble C1 Conversion to C4 compounds at 2 g/L titer

- Life cycle (LCA) and technoeconomic analysis (TEA):

• Identify cost drivers and synergies with existing technologies

Species	Rate of Formation ^a	Selectivity ^b	Energy Efficiency ^c	Current TRL ^d
Carbon Monoxide	High	High	High	High
Ethylene	High	Medium	Low	Low
Formate	Medium	High	Medium	Low
Methane	High	High	Medium	High
Acetate	Low	High	Medium	Low
Methanol	High	High	High	High

^a High: >200 mA/cm² (or commercial TC), Medium: 200 >/>100 mA/cm², Low: <100 mA/m³
 ^b High: >80%, Medium 80% > FE > 60%, Low: < 60%
 ^c High: >60%, Medium 60% > EE > 40%, Low: < 40%
 ^d High: Operated at TRL > 6, Medium: Operated TRL 4-6, Low: Operated TRL 1-3

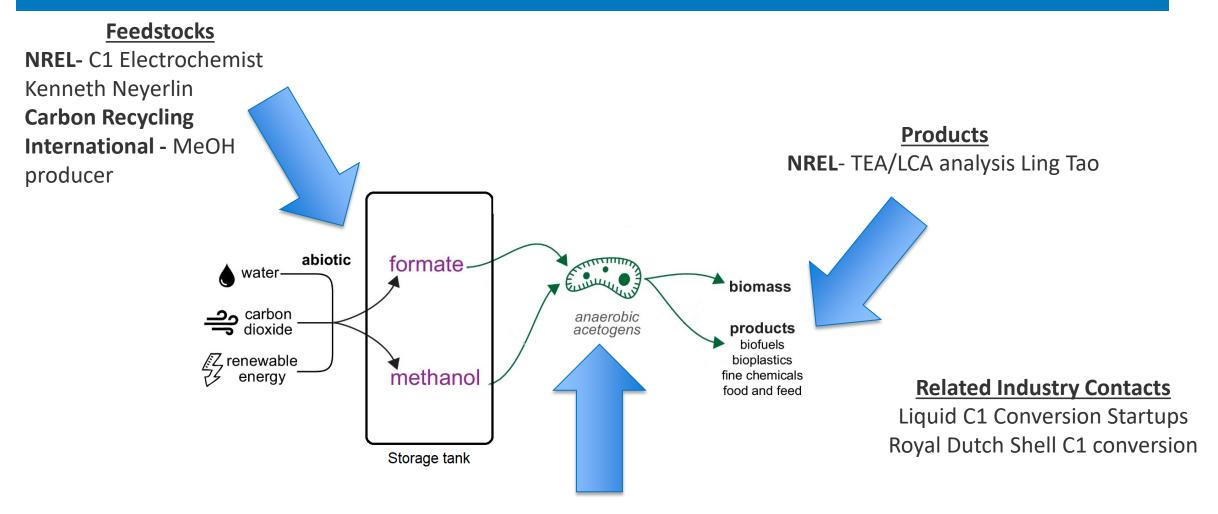
Qualitative evaluation of product ease of formation. From "Transforming the carbon economy: challenges and opportunities in the convergence of low-cost electricity and reductive CO2 utilization"

Project Overview

	Methanol category	Commercial	Feasibility and R&D
Perspective Published: 11 January 2021 An industrial perspective on catalysts for low-	Bio-methanol	 BASF (GER) BioMCN (NL) Enerkem (CAN) New Fuel (DEN) 	 Biogo (GER) Enerkem (NL) LowLands Methanol Heveskes Energy (NL) NREL (USA) Origin Materials (USA) Södra (SE)
Interfactor of the period	Renewable methanol	 CRI (IC) Innogy (GER) 	 Advanced Chemical Technologies (CAN) Asahi Kasei (JPN) Blue Fuel Energy (CAN) bse Engineering (GER) Catalytic Innovations (USA) CRI (CN/GER) Gensoric (GER) Infraserv (GER) Liquid Wind (SE) MefCO2 (GER) Neo-H2 (USA) Port of Antwerp (BE) Quantiam Technologies (CAN) STEAG (GER) Swiss Liquid Future (CH) thyssenkrupp (GER) USC (USA) ZASt (GER)
	Low carbon methanol	 GPIC (BAH) Methanex (CAN) QAFAC (QAT) SABIC (KSA) 	 Carbon2Chem (GER) FRESME (SE) GasTechno (USA) Haldor Topsoe (DEN) Maverick Synfuels (USA) NCF (CN) OPTIMeoH (GER)

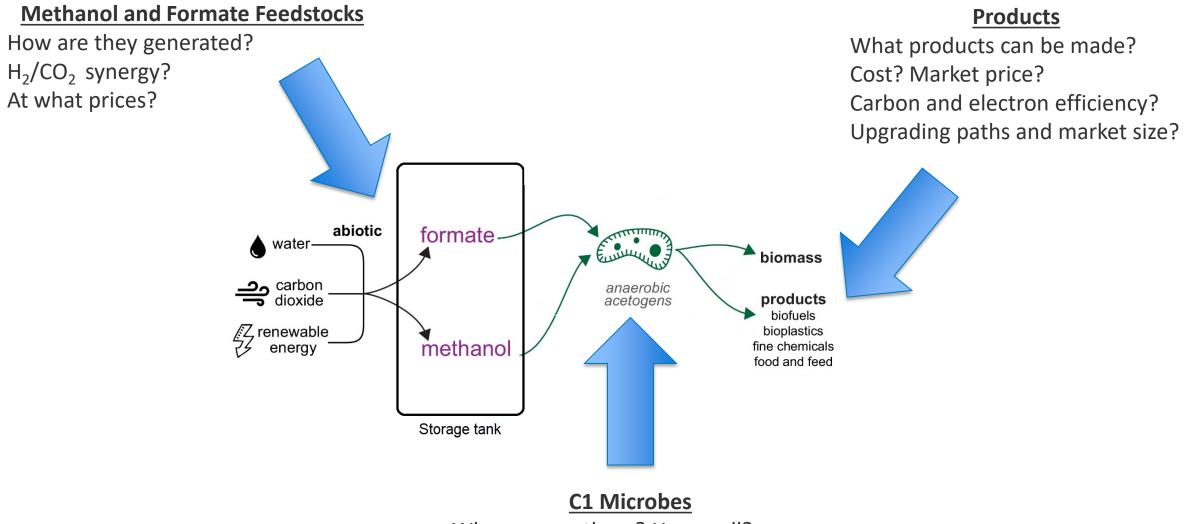
From <u>Methanol.org</u>

Management



<u>C1 Organisms</u> NREL- Microbiologist Jonathan Lo

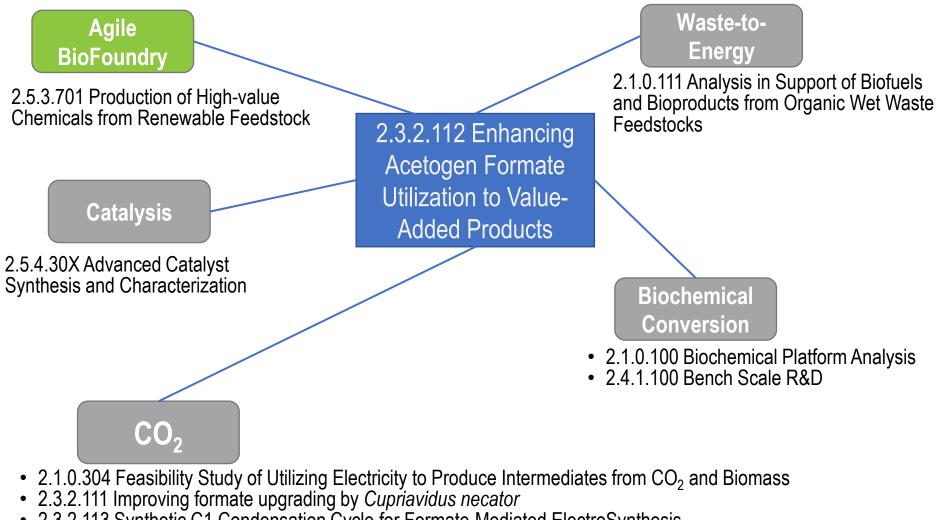
Management



Who can use them? How well? What do they make?

Can they be genetically engineered?

Approach and Management

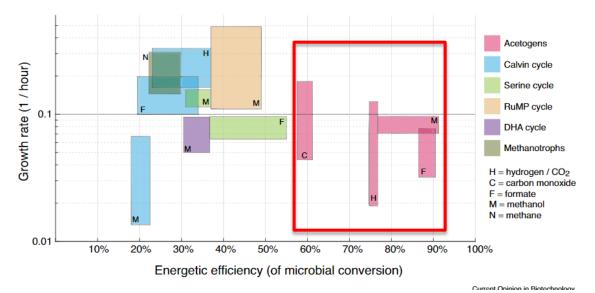


- 2.3.2.113 Synthetic C1 Condensation Cycle for Formate-Mediated ElectroSynthesis
- 5.1.3.101 Integration of CO₂ Electrolysis with Microbial Syngas; Upgrading to Rewire the Carbon Economy
 2.3.2.106 CO2 Valorization via Rewiring Metabolic Network
- Royal Dutch Shell/Princeton CO2 Conversion ACT Project

Approach: Highest biological efficiency for CO₂ fixation

Renewable methanol and formate as microbial feedstocks

Charles AR Cotton¹, Nico J Claassens¹, Sara Benito-Vaquerizo¹ and Arren Bar-Even

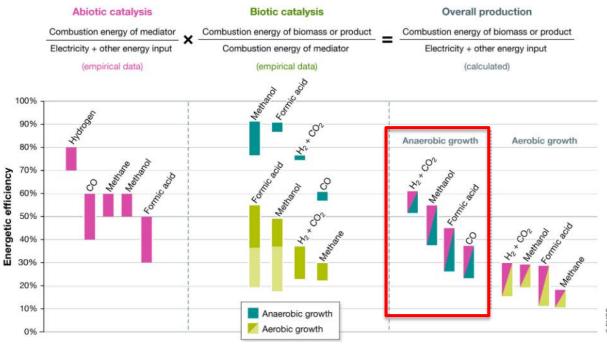


Current Opinion in Biotechnology 2020, 62:168–180

A one-carbon path for fixing CO_2

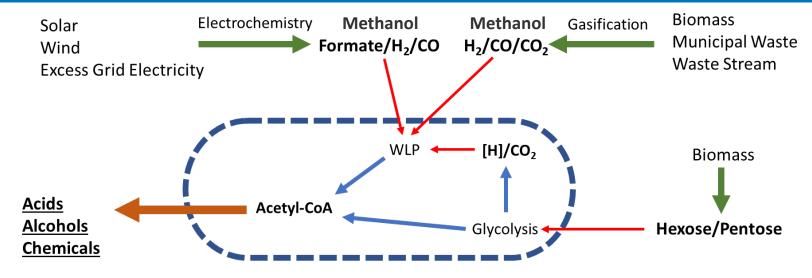
Ari Satanowski, Arren Bar-Even 💿 🎬

EMBO Rep (2020)21:e50273



"Bioproduction with acetogens is thoroughly researched and commercially exploited using gaseous C₁ feedstocks...<u>only a small</u> <u>number of acetogens have been tested for growth on methanol</u> <u>and formate...miscible carbon sources support higher energetic</u> <u>efficiencies of bioproduction</u>"

Approach: Acetogens for CO₂ fixation



Acetogens non-photosynthetically, anaerobically fix CO₂

- Use Wood Ljungdahl Pathway (WLP), most efficient for CO₂ fixation
- Investigated for syngas conversion, but can use liquid C1 formate and methanol
- Avoids gas mass transfer issue, easier to store and transport
- Can simultaneously use gases, liquids, and biomass related sugars
- Produce interesting products at high carbon and electron efficiency
- Focus on C4 products (butanol/butyrate) due to their ease of upgrading to fuels

Approach - Milestones

• Transform C4 overexpression pathway into acetogen to boost yield of C4 products (Q1)

- Growth ≥1L reactor for TEA/LCA metrics analysis (Q2)
- TEA/LCA analysis of butanol/butyrate production with different feedstock mixes to determine cost drivers, carbon efficiencies, product separation, purification, and upgrading (Q3)

End goal

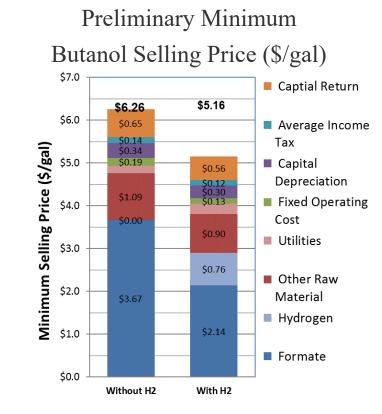
• <u>Proof of concept</u>: Demonstrate production of 2 g/L of a C4 compound in an engineered acetogen using 1-carbon feedstocks (Q4)

Progress and Outcomes TechnoEconomic Analysis

Assumptions for CO₂ Reduction to Formate

1 2	
Parameters	Value
Cell Voltage (V)	2.08
Current Density (mA/cm ²)	300
Faradaic Efficiency (%)	95
CO ₂ Single-pass Conversion (%)	90
CO Faradaic Efficiency (%)	0
H ₂ Faradaic Efficiency (%)	5
Electrolyzer Capital Cost (\$/m ²)	10,000
Electricity Price (\$kWh)	0.03
CO Market Price (\$/kg)	0.23
H ₂ Price (\$/kg)	1.57
Water Price (\$/kg)	0.00022
CO ₂ Capture Price (\$/ton)	20

- Formate is a poor electron source
- H₂ improves Carbon yield
- Butyrate versus butanol?
- Methanol is cheap, electron rich, soluble
- From methane or electrochemically
- Potential cosubstrate
- C1 miscible

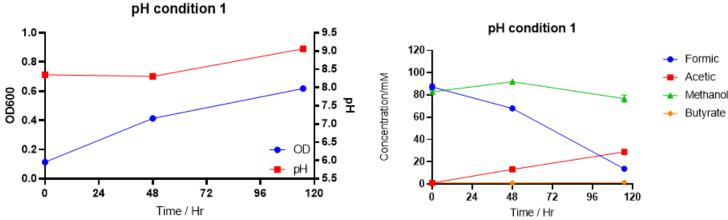


Equation	[C] Yield	Mass Yield
$C_6H_{12}O_6$ (sugar) $\rightarrow C_4H_{10}O_2$ (butanol) + 2 CO_2 + H_2	0.67	0.41
12 CH_2O_2 (formate) $\rightarrow C_4H_{10}O$ (butanol) + 8 CO_2 + 7 H_2O	0.33	0.13
7 CH_2O_2 (formate) +5 $H_2 \rightarrow C_4H_{10}O$ (butanol) + $3CO_2$ + $7H_2O$	0.57	0.23
4 CH_2O_2 (formate) +8 $H_2 \rightarrow C_4H_{10}O$ (butanol) + 7 H_2O	1.00	0.40

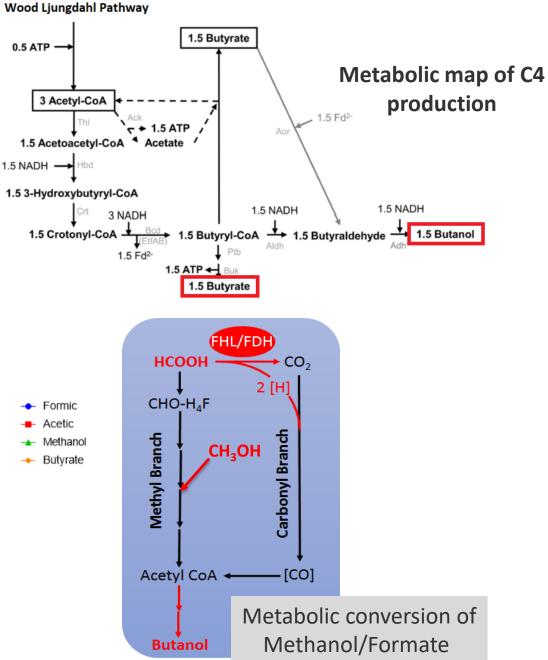
	USD/kg \$	MW	Mass yield g/g	Input cost \$ per kg	% Cost reduction
Methanol	\$0.29	32.04	0.58	\$0.49	
Glucose	\$0.29	180.16	0.41	\$0.70	30%
Butanol	\$1.20	74.12			

Progress and Outcomes C1 conversion

- <u>Butyribacterium methylotrophicum (Bm)</u>
 - Can use formate/methanol alone
 - No genetic tools
 - No metabolic models
 - Acetate/ethanol/butyrate/butanol

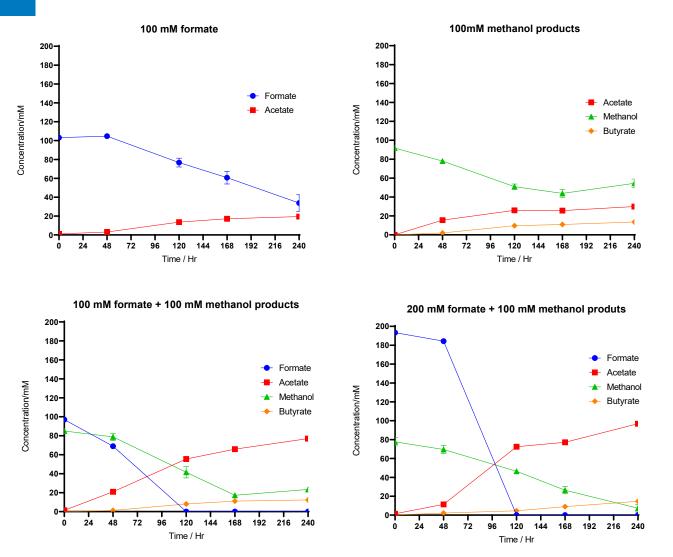


Growth and production on formate/methanol



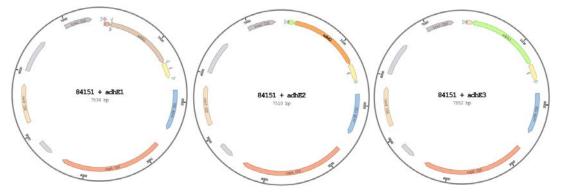
Progress and Outcomes C1 conversion specifics

- **Bm** can naturally make C4 (butyrate/butanol)
 - 100 mM formate 200 mM MeOH
 - 41 mM (3.6 g/L) butyrate
- Methanol seems to drive formation for butyrate, but does not make butanol
- Different C1 mixtures and conditions for different product formation
- Single substrate C1 fermentation is slow
- C1 mix is synergistic
 - Tolerance (~500mM formate, >1M methanol)
 - Consumption kinetics (yields, rates, titers)

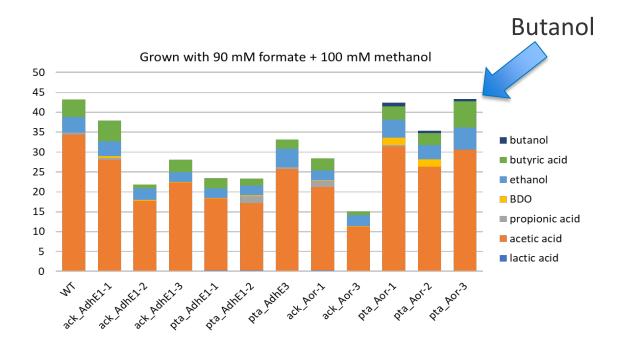


Progress and Outcomes Organism development

- Genetics tools development
 - Protocol established
 - Building CRISPR/Cas9 plasmids
 - Butanol production strategies
 - Promoter testing
- Metabolic analysis
 - RNAseq analysis
 - Substrate specificity
 - Product profile
 - Linking genes to products



Plasmids expressing different alcohol dehydrogenases (AdhE). AdhE is known to convert aldehydes into alcohols and is needed to create ethanol and butanol.



Growth of *B. methyltrophicum* engineered strains on 90 mM formate and 100 mM methanol.

Progress and Outcomes Organism development

- Test tube scale
 - 3.6 g/L butyrate
 - 50% Carbon efficiency
- Bioreactor scale up
 - Fermentation control
 - Experimenting with conditions
 - Feeding strategies
 - Improving yield/rate/titer
 - Capturing metrics for second TEA/LCA analysis



Impact – Data and Dissemination

- Direct CO₂ conversion to C1 chemicals has a high technology readiness level, but C1 chemicals have a low market price.
- Larger compounds C2-C4 have a higher value
- Direct contact with <u>Royal Dutch Shell</u>, and renewable Methanol <u>Carbon Recycling</u> <u>International (CRI)</u>
- Several forthcoming publications around microbial C1 conversion.
 - Genetic engineering and describing metabolism
 - Describing techniques, new tools, analysis
 - Metrics regarding C1 fermentation
 - Yield/rate/titer, fermentation strategies to change products
 - Fermentation process using real liquid C1s from CO₂

Feedstocks		USD/kg	\$/mole
C1	Methanol	\$0.29	\$0.009
C1	CO2	\$0.00	\$0.000
C1	Formate	\$1.00	\$0.046
Products		USD/kg	\$/mole
C2	Acetate	\$0.80	\$0.048
C4	Butyrate	\$1.50	\$0.132

Feedstock and product market costs.

Impact – Future Work

- Liquid C1 fermentation strategies
 - Implementing real CO₂ reduction streams
 - Fed batch, continuous, in situ extraction
 - Supplement CO/H_2 for better growth and carbon efficiency?
- Direct production of methanol conversion to C4?
 - Methanol is cheap (\$276/MT), readily available, derived from methane, or electrochemically renewable from CO2 (Vulcanol).
- Engineering *B. methyltrophicum* to make C4 (butyrate /butanol) at higher yield
 - Target native pathways, adding C4 pathways, planning RNAseq experiment
 - CRISPR/Cas9 gene deletion, genomic integration
- Proposals to further develop process, explore variations, outside partner collaboration

Summary

Product

Feedstock

Capital

0	Anticipated decrease in gasoline/ethanol demand; diesel demand steady
1	Increasing demand for aviation and marine fuel
ℬ	Increasing demand for renewable/recyclable materials
0	Decreasing cost of renewable electricity
P	Sustainable waste management
6.8	Expanding availability of green H ₂
	Closing the carbon cycle
	Challenges and costs of biorefinery start-up
\$	
0	Carbon intensity reduction

NREL's Bioenergy Program Is Enabling a Sustainable Energy Future by Responding to Key Market Needs

Value Proposition

 CO₂ conversion to liquid C1 for microbial upgrading represents an interesting proposition for renewable energy integration with CO₂ as a feedstock

Key Accomplishments

- Identified and developed microbial C1 conversion to C2 and C4 products
- Developed a TEA/LCA analysis for understanding the process
- Filling in knowledge gaps and disseminating knowledge among academic and industry institutions

NREL

- Jonathan Humphreys
- Lauren Magnusson
- Holly Rohrer
- Yi Pei Chen
- Wei Xiong
- Ling Tao
- KC Neyerlin
- Pin Ching Maness

Thank You

www.nrel.gov

NREL/PR-2700-79300

Jonathan.Lo@nrel.gov

Program 2.3.2.112

This work was authored by the National Renewable Energy Laboratory, operated by Alliance for Sustainable Energy, LLC, for the U.S. Department of Energy (DOE) under Contract No. DE-AC36-08GO28308. Funding provided by the U.S. Department of Energy Office of Energy Efficiency and Renewable Energy Bioenergy Technologies Office. The views expressed in the article do not necessarily represent the views of the DOE or the U.S. Government. The U.S. Government retains and the publisher, by accepting the article for publication, acknowledges that the U.S. Government retains a nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form of this work, or allow others to do so, for U.S. Government purposes.



Responses to Previous Reviewers' Comments

This project aims to convert formate to butanol using Clostridia ljungdahlii. Formate is one of the target intermediates that can be produced via chemical synthesis. It is not clear whether butanol is the best target product considering their value and subsequent separation issues etc. Thus, a better system engineering should be incorporated to fully evaluate the proposed technology.

<u>Response</u>: The TEA analysis is utilized to evaluate which products could best be made from formate. In our system, formate is first converted into acetyl-CoA, which is a precursor to many other products that could be made instead of formate, including ethanol, buytrate, and mevalonate, which could be made instead of butanol.

As a benchmark, assuming 100% formate conversion and 3 V for the electrochemical cell producing formate, the electricity demand will be ~26 kWh per kg butanol. The energy demand for state-of-the-art formate producing cells is substantially more than the thermodynamic minimum. Even if electricity is cheap, the extra cost of an inefficient energy conversion may make the process uncompetitive.

Response: Having high conversion to product is an important consideration for reaching economically feasible. It may be that we need higher efficiency of formate conversion to products, and that may be through co feeding other substrates like H2/CO to better efficiencies so that the formate carbon and electrons are better matched towards products.

Publications, Patents, Presentations, Awards, and Commercialization

We anticipate at least 2 publications from this project in progress:

Butyribacterium methylotrophicum C1 liquid conversion characterization via RNAseq analysis and bioreactor data

Development and Genetic Engineering of *Butyribacterium methylotrophicum* as a chassis organism for conversion of C1 compounds to Value Added products