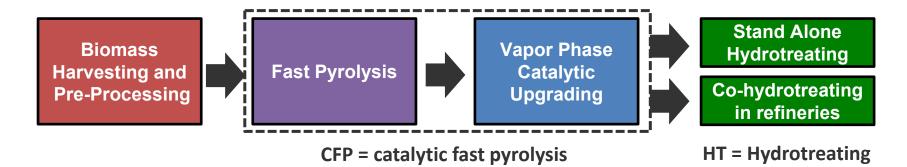


Transforming **ENERGY**

Co-Hydrotreating of Catalytic Fast Pyrolysis Oils with Straight-Run Diesel

Kristiina Iisa, Kellene Orton, Calvin Mukarakate, Abhijit Dutta, Joshua Schaidle, Michael Griffin, Luke Tuxworth, Mike Watson TCBiomass April 21st, 2022

Catalytic Fast Pyrolysis (CFP) Oil Hydrotreating



- Co-hydrotreating of CFP oil in a petroleum refinery offers several potential advantages
 - Reduces cost by enabling utilization of larger scale of petroleum refineries
 - Simplified process at biorefinery
 - Introduces biogenic carbon into refinery
- Introduces significant technical risk to refineries
 - Product quality
 - Plugging and fouling, corrosion

Standalone vs. Co-Hydrotreating

Standalone	hydrotreating	g of CFP oil
------------	---------------	--------------

- Process, catalyst and conditions can be developed to optimize CFP oil hydrotreating
- Need to generate product suitable as blendstock or further processing
- High temperature: 400°C
- High pressure: 125 bar
- Low liquid hourly space velocity (LHSV): 0.2 L/(L h)

Co-hydrotreating

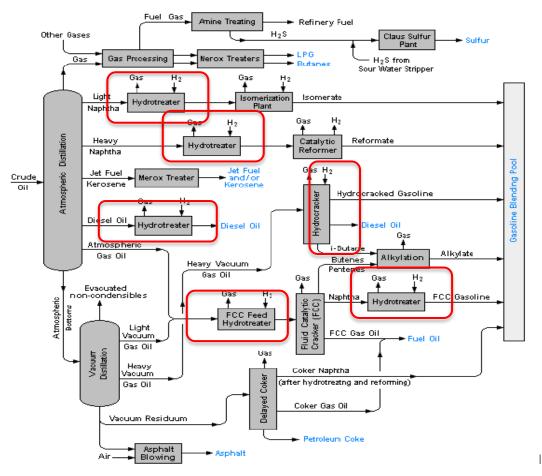
- Need to be performed at petroleum operating conditions and with petroleum catalyst
- Cannot interfere with efficiency of petroleum operation or product quality
- Lower temperatures: ~325°C
- Lower pressures: 60 bar
- Higher liquid hourly space velocity (LHSV): 1-2 L/(L h)

Limited information on co-hydrotreating of CFP oil

- CFP oil deoxygenation efficiency at co-hydrotreating conditions?
- Impact of CFP oil addition on petroleum stream transformations?
- Carbon incorporation from CFP oil?

Co-Hydrotreating in Refineries

- Petroleum refineries contain several hydroprocessing units
 - Typically for denitrification and desulfurization
 - Same catalysts active for deoxygenation
- We chose diesel hydrotreating
 - Projected continued steady demand for diesel
 - Hydrotreated CFP oil volatility



Experimental

- CFP oil produced from woody biomass (pine and forest residues) over a bifunctional metal-acid catalyst (Pt/TiO₂) in the presence of added hydrogen
 - Bifunctional CFP catalyst enables hydrogenation of coke precursors
 - \rightarrow higher oil carbon yield for CFP step

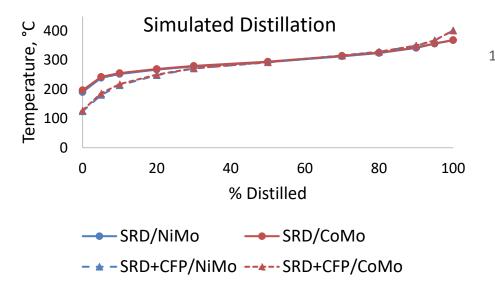
Property	Value		
C, wt% db	76.4%	30	
H, wt% db	7.8%		
O, wt% db	15.6%	20	
N, wt% db	0.2%	≈ ²⁰	
H ₂ O, wt%	2.8%	>	
TAN, mg KOH/g	217	10	
CAN, mg KOH/g	39		
Carbonyls, mol/kg	1.7	0	

Hydrotreating Catalyst: NiMo vs CoMo

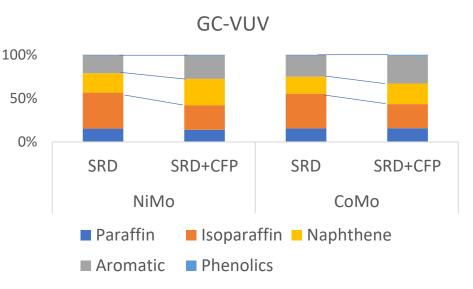
- 80 vol% Pt/TiO₂ CFP oil + 20 vol% straight-run diesel (SRD)
- Operating conditions: 325°C, 55 bar, 1 g/(g cat h)
- Catalyst: sulfided NiMo/Al₂O₃ or CoMo/ Al₂O₃

Feed	Cat.	Composition, wt%		H ₂	Mass Yields		C Yields		ICN			
		0	Ν	S	%	Oil	Aq.	Gas	Oil	Aq.	Gas	
SRD		0.2	0.03	0.21								
CFP Oil		17.5	0.18	0.01								
SRD	NiMo	≤0.3	0.03	0.01	0.1	100	-	0.3	100	-	0.3	50
SRD+CFP	NiMo	≤0.3	0.04	0.03	1.4	94	5.4	1.4	100	0.1	1.3	45
SRD	СоМо	≤0.3	0.02	0.02	0.0	101	-	0.0	101	-	0.0	48
SRD+CFP	СоМо	≤0.3	0.04	0.04	1.1	91	6.0	1.4	95	0.1	1.4	42

Hydrotreating Catalyst: NiMo vs CoMo



- SRD + CFP gave more of low-boiling products
- No difference between NiMo and CoMo



- SRD + CFP enhanced aromatics and naphthenes
- NiMo gave lower aromatics

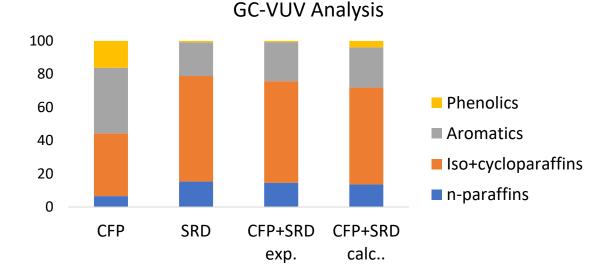
Standalone vs Co-hydrotreating over NiMo

- Co-hydrotreating 80 vol% CFP oil + 20 vol% straight-run diesel (SRD) vs
- Standalone hydrotreating of CFP oil and SRD
- Operating conditions: 325°C, 55 bar, WHSV 1 h⁻¹, sulfided NiMo

Feed	CFP	SRD	SRD+CFP experimental	SRD+CFP calculated			
Mass Yields, g/g CFP oil							
Oil	85%	100%	96%	97%			
Aqueous	16%	0.0%	5.5%	3.6%			
Gas	5.8%	0.3%	1.4%	1.5%			
H ₂ consumption	3.6%	0.1%	1.4%	0.9%			
Oil C Yield	94%	99%	99%	98%			
Product O content	8.2%	<0.1%	0.1%	1.9%			

• Co-hydrotreating suggests better deoxygenation than by standalone hydrotreating at the same condition

Standalone vs Co-hydrotreating over NiMo



• GC-VUV analysis also suggests lower oxygenates than predicted from standalone hydrotreating

Fuel Properties and Biogenic Carbon

- Co-hydrotreating 90 vol% CFP oil + 10 vol% straight-run diesel (SRD)
- Operating conditions: 340°C, 83 bar, 1 g oil/(g cat h), sulfided NiMo
- Fractionated product and measured fuel properties

Fraction	Atmospheric equivalent temp., °C	Mass fraction	Indicated cetane number (ICN)	Cloud point, °C
Gasoline	<182	6%		
Diesel	182-330	85%	50	-19
Residue	>330	9%		

- C 14 analysis of whole hydrotreated product: 9.5% biogenic carbon
 - 95% of carbon in CFP oil incorporated in product

Fuel Cut Properties and Biogenic Carbon

- Co-hydrotreating 90 vol% CFP oil + 10 vol% straight-run diesel (SRD)
- Operating conditions: 340°C, 83 bar, 1 g oil/(g cat h), sulfided NiMo
- Fractionated product and measured fuel properties

Fraction	Atmospheric equivalent temp., °C	Mass fraction	Indicated cetane number (ICN)	Cloud point, °C	Fraction biogenic carbon
Gasoline	<182	6%			40%
Diesel	182-330	85%	50	-19	4.7%
Residue	>330	9%			7.0%

- C 14 analysis of whole hydrotreated product: 9.5% biogenic carbon
 - 95% of carbon in CFP oil incorporated in product

Conclusions

- Co-hydrotreating of catalytic fast pyrolysis oil together with straight-run diesel:
 - NiMoS_x more desirable HT catalyst than CoMoS_x
 - Good deoxygenation
 - Oxygen content in hydrotreated product below detection limit
 - Enhanced deoxygenation compared to standalone hydrotreating under similar conditions
- High carbon incorporation in fuel product
 - Overall, 95% C incorporation from CFP oil into hydrotreated product
 - Gasoline-range product enriched in CFP oil
- Opportunities to improve performance
 - C-C coupling to increase fraction in diesel range
 - Co-product formation from lighter compounds
 - Recycle to decrease residue fraction

Acknowledgements

- U.S. DOE BETO for funding
- NREL
 - Kellene Orton, Sean West, Andy Young, Alex Rein
 - Calvin Mukarakate, Scott Palmer, Carson Pierce, Rick French
 - Earl Christensen, Jon Luecke, Lisa Fouts
 - Mike Griffin, Josh Schaidle
- Johnson Matthey Technology Center
 - Luke Tuxworth
 - Mike J. Watson

Acknowledgements

Please visit our related presentations on CFP and hydrotreating

- Sustainable Aviation Fuel via Hydroprocessing of Catalytic Fast Pyrolysis Oil
 - Wednesday 11:15
- Improving Process Durability by Addressing Catalyst Deactivation During Upgrading of Biomass Pyrolysis Vapors
 - Wednesday 1:30
- Co-hydrotreating of Catalytic Fast Pyrolysis Oils with Straight-Run Diesel
 - Thursday 2:00
- Advancement of the Catalytic Fast Pyrolysis of Biomass Technology with Fixed-bed Reactor to Produce Renewable Fuels and Chemicals (poster)
- Techno-Economic Analysis of Fixed Bed Ex-Situ Catalytic Fast Pyrolysis Using a Pt/TiO2 Catalyst for the Production of Fuels and Oxygenated Co-Products (poster)
- Comparative analysis of catalytic and non-catalytic pyrolysis oil co-processing by hydroprocessing and fluid catalytic cracking (Poster)

Thank you!

www.nrel.gov

NREL/PR-5100-82694

This work was authored by the National Renewable Energy Laboratory, operated by Alliance for Sustainable Energy, LLC, for the U.S. Department of Energy (DOE) under Contract No. DE-AC36-08GO28308. Funding provided by the U.S. Department of Energy Office of Energy Efficiency and Renewable Energy Bioenergy Technologies Office. The views expressed in the article do not necessarily represent the views of the DOE or the U.S. Government. The U.S. Government retains and the publisher, by accepting the article for publication, acknowledges that the U.S. Government retains a nonexclusive, paid-up, irrevocable, worldwide license to publish or reproduce the published form of this work, or allow others to do so, for U.S. Government purposes.

