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**NISTIR 3969**

# **A SURVEY OF CURRENT WORLDWIDE RESEARCH ON THE THERMOPHYSICAL PROPERTIES OF ALTERNATIVE REFRIGERANTS**

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June 1991

Sponsored by  
U.S. Department of Energy  
Office of Buildings and Community Systems  
1000 Independence Ave., SW  
Washington, DC 20585



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U.S. DEPARTMENT OF COMMERCE, Robert A. Mosbacher, Secretary  
NATIONAL INSTITUTE OF STANDARDS AND TECHNOLOGY, John W. Lyons, Director



## ABSTRACT

This survey represents an exhaustive compilation of the research activities throughout the world concerned with either measurements or correlations of the thermophysical properties of alternative refrigerants. The properties covered in this study include thermodynamic, transport, phase equilibria, and other properties such as dielectric constant and refractive index. This survey has included a wide range of fluids (including R23, R32, R125, R143a, R22, R134a, R152a, R134, R124, R142b, R123, R123a, R141b), along with mixtures containing at least one of these fluids. This report presents in tabular form summary information about each research activity; this survey does not present raw data or correlating equations.

Key words: hydrochlorofluorocarbons; hydrofluorocarbons; refrigerants; survey; thermodynamic properties; thermophysical properties; transport properties



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## INTRODUCTION

The advent of the Montreal Protocol banning the future production of the fully halogenated chlorofluorocarbon (CFC) refrigerants, which are major contributors to the environmental problems of ozone depletion and greenhouse warming, has presented a major challenge to the refrigeration industry. The expected prospect of also phasing out hydrochlorofluorocarbons (HCFCs) sometime early in the next century adds to this challenge. There are a number of very promising fluids under study which may serve as substitutes, either as pure fluids, as constituents of mixtures, or both. These substitutions must not, however, be done at the expense of energy efficiency. In order to evaluate the performance (energy efficiency, capacity, etc.) of these fluids in any thermodynamic cycle, a knowledge of their thermophysical properties is required. Accurate values of these properties are essential to select, from a set of closely related fluids or fluid mixtures, the working fluid that will yield the highest energy efficiency in refrigeration and heat-pumping applications.

The results of a comprehensive survey of current worldwide research on the thermophysical properties of alternative refrigerants are reported here in tabular form. This work summarizes under a single cover an exhaustive compilation of these activities. Its objectives are (1) to assist in the coordination of existing research programs so as to expedite the acquisition of the required property data and to not unnecessarily duplicate research programs and (2) to serve as a guide for planning the future directions of research projects involving the thermophysical properties of alternative refrigerants.

The traditional approach to determining the thermophysical properties of a given fluid is an exacting, time-consuming, and specialized endeavor. In order to expedite the effort to achieve an accurate knowledge of the thermophysical properties of environmentally acceptable refrigerants, it was appropriate to establish an international collaborative effort to provide a forum for the exchange of information and data and for the coordination of activities. Toward this end, the Advanced Heat Pump Programme of the International Energy Agency established Annex 18: "Thermophysical Properties of the Environmentally Acceptable Refrigerants." The ultimate goal of this Annex is to provide property formulations that will become de facto international standards for the most promising candidates. The first step necessary to accomplish this goal is to identify the sources of experimental data and correlations. Therefore, this report of current research activities on the thermophysical properties of alternative refrigerants represents the first major task of Annex 18. This report presents in tabular form the results of this task; this survey will be updated as deemed necessary by the development of new research activities in this area.

This survey represents an exhaustive compilation of the research activities throughout the world concerned with either measurements or correlations of the thermophysical properties of alternative refrigerants. The properties covered in this study include thermodynamic, transport, phase equilibria, and other properties such as dielectric constant and refractive index. This survey has covered a wide range of fluids (including R23, R32, R125, R143a, R22, R134a, R152a, R134, R124, R142b, R123, R123a, R141b), along with mixtures containing at least one of these fluids. These fluids are listed with their molecular mass, normal boiling point, etc. in Table 1. This report presents in tabular form summary information about each research activity; this survey does not present raw data or correlating equations. Future IEA collaborative tasks include the measurement, compilation, and evaluation of experimental data for the most important alternatives, along with the development and recommendation of correlations.

Table 1—Summary of Alternative Refrigerants

Fluid number	formula	MW (g/mol)	NBP (°C)	T <sub>c</sub> (°C)
R23	CHF <sub>3</sub>	70.01	-82.1	25.9
R32	CH <sub>2</sub> F <sub>2</sub>	52.02	-51.8	78.4
R125	CF <sub>3</sub> CHF <sub>2</sub>	120.02	-48.6	66.3
R143a	CF <sub>3</sub> CH <sub>3</sub>	84.04	-47.4	73.1
R22	CHClF <sub>2</sub>	86.47	-40.8	96.2
R134a	CF <sub>3</sub> CH <sub>2</sub> F	102.03	-26.1	101.1
R152a	CHF <sub>2</sub> CH <sub>3</sub>	66.05	-24.2	113.3
R134	CHF <sub>2</sub> CHF <sub>2</sub>	102.03	-19.4	119.0
R124	CHClFCF <sub>3</sub>	136.48	-12.1	122.5
R142b	CClF <sub>2</sub> CH <sub>3</sub>	100.50	-9.3	137.1
R123	CHCl <sub>2</sub> CF <sub>3</sub>	152.93	27.9	183.8
R123a	CHClFCClF <sub>2</sub>	152.93	29.8	185.8
R141b	CCl <sub>2</sub> FCH <sub>3</sub>	116.95	32.0	204.7

## SURVEY PROCEDURE

The survey was conducted by Annex 18 participants from Japan, the United Kingdom, and the United States, with the U.S. participants acting as overall coordinators. A comprehensive survey form (Figure 1) was developed and in the early summer of 1990 was sent to over 120 research groups worldwide that were either known to be active in refrigerant research or that have fluid property expertise. Responses were received from more than 60 research groups in 15 countries. Additional responses were received but were not included in the summary presented here because the work fell outside the scope of the survey (e.g., heat transfer measurements on alternative refrigerants) or was proprietary and insufficient information was provided. Studies of refrigerant–oil solubility were not included here even though they were on the survey form; the very limited number of responses received were not felt to be representative of the extensive work in this area either because we did not query the appropriate research groups or because refrigerant–oil research is largely proprietary.

The focus of the survey is on current studies of refrigerant thermophysical properties. Also solicited in the survey and included here are recent work (i.e., work completed since 1988) and future work. Although the survey instructions specified that future work be included only if a definite commitment for funding had been established, many of the projects listed several years in the future, or simply as “planned,” probably do not meet this criterion. References for published results during the past two years are also reported.

This report has been distributed to all participants in IEA Annex 18 as well as to all survey respondents. This will hopefully facilitate the objectives of this Annex.

Name \_\_\_\_\_ Institution \_\_\_\_\_

Project type:  experimental measurement  modeling/correlation

Fluid(s) studied:

- R23     R32     R125     R143a     R22     R134a     R152a  
 R134     R124     R124a     R142b     R123     R123a     R141b

mixture--please list components and composition(s) \_\_\_\_\_

other(s)--please list \_\_\_\_\_

sample purity \_\_\_\_\_

- by own analysis     by suppliers analysis     estimated/unknown

Property(ies) measured/correlated (also indicate number of experimental points):

- vapor pressure (\_\_\_\_)     saturation density (\_\_\_\_)     critical parameters (\_\_\_\_)  
 P-V-T (\_\_\_\_)     surface tension (\_\_\_\_)     dielectric constant (\_\_\_\_)  
 heat capacity (\_\_\_\_)     sound speed (\_\_\_\_)     viscosity (\_\_\_\_)  
 thermal conductivity (\_\_\_\_)     refractive index (\_\_\_\_)     mixture V-L-E (\_\_\_\_)  
 refrigerant/oil solubility (\_\_\_\_)  
 other(s)--please list \_\_\_\_\_

Experimental technique/correlating equation employed:

---

---

Estimated accuracy (experimental projects only)

---

Range of measurements/correlation (either indicate numerically or sketch below)

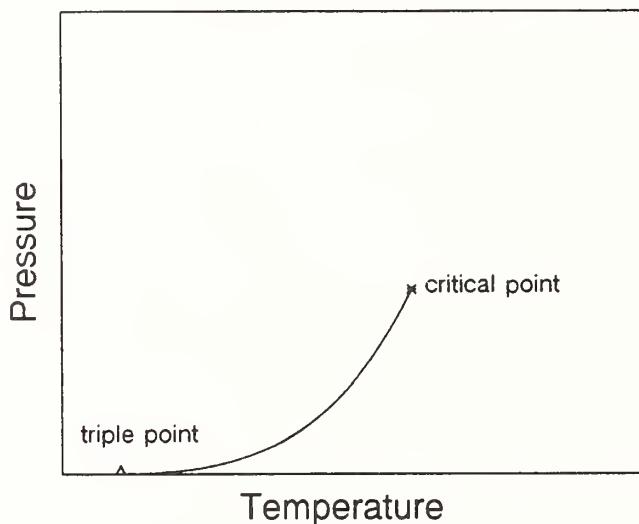
temperature: from \_\_\_\_\_ to \_\_\_\_\_

pressure: from \_\_\_\_\_ to \_\_\_\_\_

density: from \_\_\_\_\_ to \_\_\_\_\_

- phase:  saturated liquid     saturated vapor     critical region  
 single-phase liquid     single-phase vapor     supercritical region

Single-phase properties



Saturation properties

property \_\_\_\_\_

\_\_\_\_\_

property \_\_\_\_\_

\_\_\_\_\_

property \_\_\_\_\_

\_\_\_\_\_

$T_{tp}$        $T_{nbp}$        $T_c$

Project status:

- completed--if paper or report is available please give reference:
- 
- 

- in progress

beginning date \_\_\_\_\_

- planned (i.e. funded)

ending date \_\_\_\_\_

Additional remarks:

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Figure 1—Survey form

## SUMMARY OF SURVEY RESULTS

A series of tables on the following pages presents the results of the survey in a compact format. Tables 2, 3, and 4 summarize the number of projects by fluid, type of property measured, and the country in which the work is being done. These tables tally the "number of projects" for a particular combination of fluid and country, or fluid and property. Each "project" represents one property studied for one fluid by one research group. A research program involving the measurement of a single property for several fluids, several different property measurements for one fluid, or a project being carried out by more than one laboratory would be counted multiple times in computing the entries in Tables 2-4. Similarly, a project measuring only a few data points is counted the same as an exhaustive set of measurements. Thus, the total quantity of work on the alternative refrigerants is considerably less than what might initially be inferred from Tables 2-4. These tables do, however, give an indication of the countries active in studying refrigerant thermophysical properties and the relative level of effort being expended for the various alternatives.

Following the summary tables, a series of tables, one for each fluid, present details of the responses. The fluids are listed in order of increasing normal boiling point; mixtures follow the pure components and are listed first in order of the normal boiling point of the more volatile component, and then by the normal boiling point of the other constituent(s). For a given fluid, the entries are further organized by property. The information presented for each entry are self-evident. Dashes indicate missing information or an item that is not applicable. The order of the entries reflects the sequence of their entry into the tables and has no other significance. Each entry is identified by the name of the person responding to the survey (usually the principal investigator), the organization, and the country. The final set of tables, organized by country, gives details on the research groups responding to this survey. Names, addresses, and telephone numbers of the principal investigator(s) and any other collaborators are given, as well as a brief listing of the techniques employed. The listing of techniques represents those that have been applied to the alternative refrigerants; in many cases these research groups have additional capabilities.

## ACKNOWLEDGMENTS

We extend our sincere thanks to all of our colleagues from around the world who shared with us information on their work on the alternative refrigerants. The U.S. participation in this task was funded by the Office of Buildings and Community Systems of the United States Department of Energy.

Table 2—Summary of Research by Fluid and Property  
(entries indicate number of projects)

Property	Fluid												other totals			
	23	32	125	143a	22	134a	152a	134	124	142b	123	123a	141b			
vapor pressure	1		2	1	5	15	7	3	2	8	15	3	6	17	4	89
sat. liquid density	1		2	2	3	10	3	4	1	5	9	2	6	9	5	62
sat. vapor density		1		2	3		1		2	4		1	2	1	17	
P-V-T	3	1	2	1	8	16	8	3	2	8	15	4	9	11	3	94
virial coefficients				1	1		1			1	1		3		8	
critical parameters		1				7	3	2	1	5	7	1	3	5	3	38
triple point par.					1	1	1			1				4		
heat capacity/calor.					1	5	2			1	2		6	2	20	
speed of sound				2	2	6	2			4	6	1	3	1	1	28
dielectric constant	2		1		3	3	2	1	1	1	3	1	2		20	
refractive index						1	2	2	2	2	1	1		1	12	
surface tension					2	4	3	2		2	6	1	1		2	
thermal conduct.				1	1	6	11	3	1	2	7	11	1	8	2	
thermal diffusivity				1		5	5	3		1	5	5		2	27	
viscosity	2	1		3	6	10	4			3	10	4	4	14	2	64
equation of state	4	4	3	3	6	9	5	4	4	4	3	3	2	11	1	63
ideal gas properties	2	2	2	2	2	2	2	2	2	2	2	2	2		26	
mixture V-L-E														24	24	
totals for fluid	16	8	17	15	53	109	51	25	16	61	101	21	50	105	25	673

Table 3—Summary of Research by Fluid and Country  
(entries indicate number of projects)

Country	Fluid										other	totals				
	23	32	125	143a	22	134a	152a	134	124	142b	123	123a	141b			
Australia											2	2	2	6		
Canada			3		3	1			2	3	2	8		25		
China					5	2			5		5			17		
Czechoslovakia					1		1							2		
France						5			5	5	5	5		25		
Germany	8	2	1	3	31	25	28	2	2	21	17	2	28	4	176	
Greece					1	1			1		1				3	
Italy						2				2					4	
Japan	1			9	4	32	7	9	5	17	38	8	13	36	4	183
Korea								3			3				6	
Portugal						3			2		3	3			12	
Sweden	2	2				2	2	2			3	3			12	
U.S.S.R.	1														1	
United Kingdom						1	4				1	2			10	
United States	5	3	13	3	11	26	11	10	9	10	20	9	21	11	17	179
total for fluid	16	8	17	15	53	109	51	25	16	61	101	21	50	105	25	673

Table 4—Summary of Mixtures Research  
 (mixture specified by intersection of pure components; table entry indicates number of projects)

## DETAILED PROJECT INFORMATION

# R23; CHF<sub>3</sub>; trifluoromethane

Property /Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
Vapor pressure Kruse; U. Hannover; FRG	l-v	--	-	--	--	--	9/89-8/91	
Saturated liquid density Kruse; U. Hannover; FRG	sl	--	-	--	--	--	9/89-8/91	
Pressure-volume-temperature Ström; Chalmers U. Tech.; Swe Zollweg; Cornell U.; USA Bier; U. Karlsruhe; FRG	l 1 v	258-323 126-332 333-423	0.5-2 sat-100 0.2-58	-- 1300 128	0.15% 0.1-0.4% 0.02-0.14%	.99 .999 .999	planned comp comp	[Rb89]
Heat capacity/calorimetry Bier; U. Karlsruhe; FRG	v	233-473	0.1-12	163	0.2%	.999	comp	
Dielectric constant Makita; Kobe U.; Japan Franck; U. Karlsruhe; FRG	l,v l,v	283-323 213-468	0.1-17 0.5-200	126 90	0.01% 0.5-1.5%	.9991 .9995	comp comp	[Rt89]
Viscosity Ström; Chalmers U. Tech.; Swe Kruse; U. Hannover; FRG	l sl,sv	258-323 --	0.5-2 -	--	2%	.99 --	planned 9/89-8/91	
Equation of State Maurer; U. Kaiserlautern; FRG Huber; NIST; USA Fischer; ORNL; USA Gallagher; NIST; USA	l,v l,v l,v l,v	203-473 all - 0.5-1.6 T <sub>c</sub>	0-58 all - 0-2 P <sub>c</sub>	- - - -	- - - -	- - - -	comp in prog comp comp	[Pl90] [El90] [Fs90] [Gl90]
Ideal Gas Properties Lucas; U. Duisburg; FRG Marsh; Texas A&M; USA	- -	100-500 0-1500	0-0 0.1	- -	1% --	- -	in prog comp	[TR90]

## Notes and References

- [El90] J. F. Ely and M. L. Huber, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 383-392.
- [Fs90] S. K. Fischer and J. Sand, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 373-382.
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- [TR90] TRC Thermodynamic Tables, Thermodynamics Research Center, Texas A&M University, continuously updated; also to be published in J. Phys. Chem. Ref. Data.

# R32; CH<sub>2</sub>F<sub>2</sub>; difluoromethane

Property /Investigator	phase	range of data T (K)	p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Pressure-volume-temperature</b>								
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	0.15%	.99	planned	
<b>Viscosity</b>								
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	2%	.99	planned	
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]
<b>Equation of State</b>								
Los; Inst. Low Temp. Engr.; USSR	v	200-500	0-5	-	-	-	6/90-10/90	
Morgenstern; HFV Dresden; FRG	l,v	190-400	0-6	-	-	-	comp	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]

## Notes and References

- [El90] J. F. Ely and M. L. Huber, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 383-392.
- [Fs90] S. K. Fischer and J. Sand, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 373-382.
- [TR90] TRC Thermodynamic Tables, Thermodynamics Research Center, Texas A&M University, continuously updated; also to be published in J. Phys. Chem. Ref. Data.

R125; CHF<sub>2</sub>CF<sub>3</sub>; pentafluoroethane

Property /Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
Vapor pressure								
Holste; Texas A&M U.; USA	l-v	230-480	-	--	0.1%	--	9/90-10/91	
Morrison; NIST; USA	l-v	268-339	-	10	-	.993	comp	
Saturated liquid density								
Holste; Texas A&M U.; USA	s l	230-480	-	--	0.1%	--	9/90-10/91	
Morrison; NIST; USA	s l	268-339	-	10	-	.993	comp	
Saturated vapor density								
Holste; Texas A&M U.; USA	s v	230-480	-	--	0.1%	--	9/90-10/91	
Pressure-volume-temperature								
Holste; Texas A&M U.; USA	l, v	230-480	0-70	--	0.1%	--	9/90-10/91	
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.993	comp	
Critical parameters								
Holste; Texas A&M U.; USA	T,P, $\rho$	-	-	-	0.1%	--	9/90-10/91	
Dielectric constant								
Morrison; NIST; USA	v	298-433	0.04-1.4	-	$3 \times 10^{-6}$	.993	comp	[My90]
Thermal conductivity								
Venart; U. New Brunswick; Canada	l, v	203-393	0.1-70	--	1%	--	planned	
Thermal diffusivity								
Venart; U. New Brunswick; Canada	l, v	203-393	0.1-70	--	5%	--	planned	
Viscosity								
Snelson; NRC; Canada	s l	253-353	-	15	2.5-3.5%	-	3/91-10/91	
Equation of state								
Huber; NIST; USA	l, v	all	all	-	-	-	in prog	[El90]
Fischer; ORNL; USA	l, v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l, v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gi90]
Ideal Gas Properties								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

Notes and References

- [El90] J. F. Ely and M. L. Huber, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 383-392.
- [Fs90] S. K. Fischer and J. Sand, Proc. ASHRAE-Purdue CFC Conference, W. Lafayette, IN, USA, July, 1990, pp 373-382.
- [Gi90] J. Gallagher, M. McLinden, and G. Morrison, National Institute of Standards and Technology, Standard Reference Data Base 23 (1990).
- [My90] C. W. Meyer and G. Morrison, J. Phys. Chem. (in press).
- [TR90] TRC Thermodynamic Tables, Thermodynamics Research Center, Texas A&M University, continuously updated; also to be published in J. Phys. Chem. Ref. Data.

R143a; CH<sub>3</sub>CF<sub>3</sub>; 1,1,1-trifluoroethane

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
Vapor pressure Widiatmo; Keio U.; Japan	l-v	200-345		-	--	10kPa	--	7/90-3/91
Saturated liquid density C. Yokoyama; Tohoku U.; Japan Widiatmo; Keio U.; Japan	s1	250-340		-	--	0.3%	.999	comp
	s1	200-345		-	--	0.2%	--	7/90-3/91
Pressure-volume-temperature Widiatmo; Keio U.; Japan	l	280-315	sat-2	--	0.2%	--	7/90-3/91	
Speed of sound Kohler; Ruhr U.;FRG Takagi; Kyoto Inst. Tech.; Japan	v	230-350	0.02-0.5	400	0.01%	.993	?/88-?/91	
	l	280-370	sat-75	100	0.2%	.9996	comp	
Thermal conductivity Tanaka; Kobe U.; Japan	v	293-353	0.1-sat	30	2%	.999	comp	[Tn90]
Viscosity Takahashi; Tohoku U.; Japan Kumagai; Tohoku U.; Japan Tanaka; Kobe U.; Japan	v	298-423	0.1-9	107	0.3%	.999	comp	[Tk90]
	s1	273-323	sat	6	0.5%	.999	comp	[Km90]
	v	283-323	0.1-0.1	5	1%	--	comp	[Ko89]
Equation of State Morgenstern; HFV Dresden; FRG Huber; NIST; USA Fischer; ORNL; USA	l,v	200-400	0-4	-	-	-	comp	
	l,v	all	all	-	-	-	in prog	[El90]
	l,v	-	-	-	-	-	comp	[Fs90]
Ideal Gas Properties Lucas; U. Duisburg; FRG Marsh; Texas A&M; USA	-	100-500	0-0	-	1%	-	in prog	
	-	0-1500	0.1	-	--	-	comp	[TR90]

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R22; CHClF<sub>2</sub>; chlorodifluoromethane

Property	Investigator	phase	range of data T (K)	p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Vapor pressure</b>									
	Blanke; PTB; FRG	l-v	113-369	-	18	0.1%	.9999	10/86-9/90	
	Gorenflo; U. Paderborn; FRG	l-v	293-369	-	33	0.04%	.9999	comp	[Rt89]
	Kohler; Ruhr U.; FRG	l-v	313-368	-	40	--	.9996	comp	[Kh90]
	Straub; T.U. München; FRG	l-v	318-374	-	50	0.5-1.5%	.9998	comp	
	Wagner; Ruhr U.; FRG	l-v	180-340	-	45	0.05%	.99995	comp	[Wg90]
<b>Saturated liquid density</b>									
	Gorenflo; U. Paderborn; FRG	s1	293-366	-	16	0.04%	.9999	comp	[Rt89]
	Wagner; Ruhr U.; FRG	s1	115-340	-	42	0.02%	.99995	comp	[Wg90]
	Kruse; U. Hannover; FRG	s1	233-353	-	8	0.3%	--	comp	
<b>Saturated vapor density</b>									
	Gorenflo; U. Paderborn; FRG	sv	293-366	-	16	0.2%	.9999	comp	[Rt89]
	Wagner; Ruhr U.; FRG	sv	250-330	-	4	0.02%	.99995	comp	[Wg90]
<b>Pressure-volume-temperature</b>									
	Blanke; PTB; FRG	l	113-470	sat-30	300	0.1%	.9999	10/86-9/90	
	Kohler; Ruhr U.; FRG	l,v	250-500	0.1-60	280	0.05%	.9996	comp	[Kh90]
	Straub; T.U. München; FRG	l,v	318-413	2-12	300	0.5-1.5%	.9998	comp	
	Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	0.15%	.99	planned	
	Wagner; Ruhr U.; FRG	l,v	120-340	0-8	55	0.02%	.99995	comp	[Wg90]
	Kubota; Kobe U.; Japan	v	348-423	0.1-11	56	0.4%	.999	comp	
	Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	--	comp	
	Sandarusi; NIST; USA	l,v	318-473	1.4-40	400	0.1-0.3%	.999+	in prog	
<b>Virial coefficients</b>									
	Schramm; Phys. Chem. Inst.; FRG	v	233-296	--	9	2%	--	comp	[Nt89]
<b>Triple point temperature</b>									
	Blanke; PTB; FRG	-	-	-	-	--	.9999	10/86-9/90	
<b>Heat capacity/calorimetry</b>									
	Sami; U. Moncton; Canada	l,v	283-353	0.5-1.4	-	2%	--	in prog	
<b>Speed of sound</b>									
	Kohler; Ruhr U.; FRG	v	230-350	0.02-0.5	400	0.01%	.9996	?/88-?/91	
	Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	0.5%	--	4/90-->	
<b>Dielectric constant</b>									
	Makita; Kobe U.; Japan	v	293-373	0.1-sat	31	0.01%	.9999	comp	
	Franck; U. Karlsruhe; FRG	l,v	233-368	0.5-200	90	0.7%	.994	comp	[Um89]
	Morrison; NIST; USA	v	298-433	0.04-1.0	-	3x10 <sup>-6</sup>	--	comp	[My90]
<b>Surface Tension</b>									
	Straub; T.U. München; FRG	l-v	223-369	-	100	0.5%	.9998	planned	
	Okada; Nagaoka U. Tech.; Japan	l-v	273-353	-	36	0.16mN/m	.9998	comp	[Ok88]

R22; CHClF<sub>2</sub>; chlorodifluoromethane (continued)

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
<b>Thermal conductivity</b>								
Assael; Aristotle U.; Greece	l,v	230-370	<40	--	0.5%	--	6/89-?	
Hemminger; PTB; FRG	v	303-463	0.1-0.1	5	2.5%	.9999	comp	[Hm89]
Stephan/Taxis; U. Stuggart; FRG	v	273-423	<5	100	1%	.99996	-->9/91	
Johns; Nat'l. Eng. Lab; UK	v	298-423	1-30	--	0.5%	--	12/90-12/92	
Perkins; NIST; USA	l,v	130-405	0.1-70	800	1%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	1%	--	in prog	
<b>Thermal diffusivity</b>								
Fiebig; Ruhr U.; FRG	l	273-363	1-8	--	1%	.995	comp	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	1-2%	--	4/90-->	
Straub; T.U. München; FRG	l,v	318-413	2-12	300	0.5-1.5%	.9998	comp	
Perkins; NIST; USA	l,v	130-405	0.1-70	800	5%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	5%	--	in prog	
<b>Viscosity</b>								
Mayinger; T. U. München; FRG	v	300-425	0.1-7.5	35	0.5%	.9995	comp	[Nb90]
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	2%	.99	planned	
Kumagai; Tohoku U.; Japan	s1	273-323	sat	6	0.5%	.999	comp	[Km90]
Kruse; U. Hannover; FRG	l	236-353	?-2.5	8	4%	.999	comp	
Diller; NIST; USA	l	120-320	sat-35	60	3%	--	comp	
Diller; NIST; USA	l,v	300-500	0.2-50	100	3%	--	10/90-10/91	
<b>Equation of State</b>								
Maurer; U. Kaiserslautern; FRG	l,v	253-473	0-35	-	-	-	comp	[Pl90]
Wagner; Ruhr U.; FRG	l,v	115-525	0-160	-	-	-	-->3/91	
Oellrich; U. Karlsruhe; FRG	l,v	-	-	-	-	-	?/89-?/92	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gl90]
Beyerlein; U. Idaho; USA	l,v	-	-	-	-	-	comp	
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

## R22; CHClF<sub>2</sub>; chlorodifluoromethane (continued)

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**R134a; CH<sub>2</sub>FCF<sub>3</sub>; 1,1,1,2-tetrafluoroethane**

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
<b>Vapor pressure</b>								
Baehr; U. Hannover; FRG	l-v	300-374	-	35	0.03%	.9993+	8/89-8/91	
Baroncini; U. Ancona; Italy	l-v	240-360	-	64	1%	.9998	comp	[Br90]
LeNeindre; U. Paris Nord; France	l-v	298-?	-	--	--	--	10/90-->	
Straub; T.U. München; FRG	l-v	318-374	-	50	0.5-1.5%	.999	1/89-8/90	
Oguchi; Kanagawa Inst. Tech.; Japan	l-v	243-374	-	37	0.5kPa	.999	comp	
Kubota; Kobe U.; Japan	l-v	253-373	-	25	3kPa	.998	comp	[Kb89]
Fukushima; Asahi Glass; Japan	l-v	262-374	-	41	5kPa	.9999	comp	
Maezawa; Keio U.; Japan	l-v	280-350	-	13	7kPa	.9999	comp	[Mz90]
Piao; Keio U.; Japan	l-v	300-374	-	51	2kPa	.995-.9999	comp	[Pi90]
Mingshan; Tsinghua U.; PRC	l-v	248-358	-	20	0.02%	.9998	comp	
Kruse; U. Hannover; FRG	l-v	--	-	--	--	--	9/89-8/91	
Howley; NIST; USA	l-v	180-360	-	19	0.03%	.9997	comp	[Hw90]
Bier; U. Karlsruhe; FRG	l-v	203-374	-	53	0.1%	.999	comp	[Bi90]
Weber; NIST; USA	l-v	313-374	-	22	0.01%	.9995	comp	[Wb89]
Morrison; NIST; USA	l-v	268-374	-	10	-	.9994	comp	[Mo90]
<b>Saturated liquid density</b>								
Baehr; U. Hannover; FRG	s1	293-373	-	9	0.1%	>.9993	8/89-8/91	
Yokoyama; Tohoku U.; Japan	s1	252-367	-	22	0.5%	.999	comp	[Yk88]
Oguchi; Kanagawa Inst. Tech.; Japan	s1	243-346	-	6	0.01-0.1%	.999	comp	
Fukushima; Asahi Glass; Japan	s1	244-374	-	16	0.2-0.3%	.9999	comp	
Maezawa; Keio U.; Japan	s1	200-370	-	25	0.2%	.9999	comp	[Mz90]
Piao; Keio U.; Japan	s1	313-372	-	7	0.15%	.995-.9999	comp	[Pi90]
Kabata; Keio U.; Japan	s1	354-374	-	11	0.5%	.995	comp	[Ka89]
Kruse; U. Hannover; FRG	s1	--	-	--	--	--	9/89-8/91	
Holste; Texas A&M U.; USA	s1	180-360	-	--	0.1%	.9997	comp	[Hi90]
Morrison; NIST; USA	s1	268-374	-	10	-	.9994	comp	[Mo90]
<b>Saturated vapor density</b>								
Kabata; Keio U.; Japan	sv	365-374	-	11	0.5%	.995	comp	[Ka89]
Fukushima; Asahi Glass; Japan	sv	271-374	-	8	3kg/m <sup>3</sup>	.9999	comp	
Weber; NIST; USA	sv	320-365	-	5	0.02%	.9995	comp	[Wb89]

R134a; CH<sub>2</sub>FCF<sub>3</sub>; 1,1,1,2-tetrafluoroethane (continued)

Property Investigator	phase	range of data T(K)	p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
Pressure-volume-temperature								
Baehr; U. Hannover; FRG	l,v	293-433	0.1-16	500	0.1%	.9993+	8/89-8/91	
Baroncini; U. Ancona; Italy	v,sv	240-360	0.1-sat	46	1%	.9998	comp	[Br90]
LeNeindre; U. Paris; France	l,v	298-413	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.3%	.995	12/89-10/93	
Straub; T.U. München; FRG	l,v	318-423	2-12	300	0.5-1.5%	.999	1/89-8/90	
Ström; Chalmers U.Tech.; Swe.	l	258-323	0.5-2	120	0.15%	.99	--	
Vacek; Czech T.U.; Czech.	l	200-300	sat-55	--	0.1%	--	6/91-12/91	
Oguchi; Kanagawa Inst. Tech.; Japan	l	243-473	0.08-17	40	0.01%	.999	comp	
Matsuо; Kobe U.; Japan	l	293-353	sat-40	50	0.02%	.999	comp	
Fukushima; Asahi Glass; Japan	l,v	320-424	1-6	63	0.2%	.9999	comp	
Maezawa; Keio U.; Japan	l	280-350	sat-2	16	0.2%	.9999	comp	[Mz90]
Piao; Keio U.; Japan	l,v	300-425	0.7-12	159	0.15%	.995-.9999	comp	[Pi90]
Mingshan; Tsinghua U.; PRC	v	248-358	0.1-6	84	0.2%	.9998	comp	
Holste; Texas A&M U.; USA	l	180-380	sat-70	300	0.1%	.9997	comp	[Hl90]
Weber; NIST; USA	v	321-423	0-5.3	69	0.02%	.9995	comp	[Wb89]
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.9994	comp	
Virial coefficients								
Schramm; Phys.-Chem. Inst.; FRG	v	233-296	--	9	2%	--	6/90-->	
Critical parameters								
LeNeindre; U. Paris; France				--	--	--	10/90-->	
Straub; T.U. München; FRG				-	0.5-1.5%	.999	1/89-8/90	
Fukushima; Asahi Glass; Japan	T,p			-	5mK,3kg/m <sup>3</sup>	.9999	comp	
Piao; Keio U.; Japan	P			-	2kPa	.995-.9999	comp	[Pi90]
Kabata; Keio U.; Japan	T,p			-	10mK,0.5%	.995	comp	[Ka89]
Kubota; Kobe U.; Japan	T,P			-	50mK,3kPa	.998	comp	[Kb89]
Bier; U. Karlsruhe; FRG				-		.999	comp	[Bi90]
Triple point temperature								
Magee; NIST; USA	-	-	-	-	--	.9995	comp	[Mg91]
Heat capacity/calorimetry								
Wormald; U. Bristol; UK	l,v	233-473	0.1-10		1%	.99+	4/90-12/91	
Piao; Keio U.; Japan	--	--	-	2	--	.995-.9999	comp	[Pi90]
Saitoh; Keio U.; Japan	l	276-356	1-3	31	0.3%	.9997	comp	[St90]
Magee; NIST; USA	l	190-340	sat-35	400	0.5%	.9995	comp	[Mg91]
Magee; NIST; USA	l,v	320-500	0.1-20	--	0.4%	.9997	10/91-12/91	
Speed of sound								
Kohler; Ruhr U.; FRG	v	230-350	.025-.5	400	0.01%	--	?/88-?/91	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	0.5%	--	4/90-->	
LeNeindre; U. Paris; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Mingshan; Tsinghua U.; PRC	v	248-358	0.1-1.5	--	0.15%	.9998	4/90-->	
Zollweg; Cornell U.; USA	l	180-380	sat-70	206	0.05%	.998	comp	[Zl90]
Goodwin; NIST; USA	v	233-340	0.02-.5*Psat	104	0.01%	.9994	comp	[Gd90]

R134a; CH<sub>2</sub>FCF<sub>3</sub>; 1,1,1,2-tetrafluoroethane (continued)

Property Investigator	phase	range of data T (K)	range of data p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Dielectric constant</b>								
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.5%	.995	12/89-10/93	
Makita; Kobe U.; Japan	v	298-348	0.1-sat	29	0.5%	.999	comp	
Morrison; NIST; USA	v	298-433	0.04-0.7	-	3x10 <sup>-6</sup>	.9994	comp	[My90]
<b>Refractive index</b>								
Straub; T.U. München; FRG	l,v	318-423	-	300	0.05%	.999	1/89-8/90	
<b>Surface Tension</b>								
Okada; Nagaoka U. Tech.; Japan	l-v	232-363		118	0.2mN/m	.9998	comp	[Ok90]
Mingshan; Tsinghua U.; PRC	l-v	263-358	-	--	--	.9998	4/90-->	
Straub; T.U. München; FRG	l-v	223-373	-	100	0.5%	.998	planned	
Schmidt; NIST; USA	l-v	263-368	-	29	0.15mN/m	.9995	comp	[Ch90]
<b>Thermal conductivity</b>								
Assael; Aristotle U.; Greece	l,v	230-370	<40	--	0.5%	--	6/89-?	
Gross/Hahne; U. Stuggart; FRG	l,v	262-354	0.1-8.0	71	1%	.998	?/88-?/92	[Gr90]
LeNeindre; U. Paris Nord; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.5%	.995	12/89-10/93	
Stephan/Taxis; U. Stuggart; FRG	v	273-423	<5	100	1%	.99+	-->9/91	
Wakeham; Imperial Col.; UK	s1,sv	260-370	sat	20	--	.999	comp	[Wk90]
Yata; Kyoto Inst. Tech.; Japan	l	250-350	sat-30	127	--	.995-.9995	comp	[Yt89]
Tanaka; Kobe U.; Japan	v	293-353	0.1-sat	33	2%	.999	comp	[Tn90]
Nagasaki; Keio U.; Japan	l	193-273	1-1	--	0.5%	.999	?/89-->	
Perkins; NIST; USA	l,v	180-410	0.1-70	800	1%	--	-->12/90	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	1%	--	planned	
<b>Thermal diffusivity</b>								
Fiebig; Ruhr U.; FRG	l	273-363	1-8	--	1%	--	1/91-->	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	1-2%	--	4/90-->	
Straub; T.U. München; FRG	l,v	318-423	2-12	300	0.5-1.5%	.999	12/89-8/90	
Perkins; NIST; USA	l,v	180-410	0.1-70	800	5%	--	-->12/90	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	5%	--	planned	
<b>Viscosity</b>								
Matthews; Polytech. S.W.; UK	v	247-573	0.01-0.1	10	0.5%	--	1/90-->	
Mayinger; T.U. München; FRG	v	300-425	0.1-6.5	41	0.5%	.9994	comp	[My90]
Ström; Chalmers U.Tech.; Swe	l	258-323	0.5-2	--	2%	.99	--	
Takahashi; Tohoku U.; Japan	v	298-423	0.1-8.8	107	0.3%	.999	comp	[Tk90]
Kumagai; Tohoku U.; Japan	s1	273-343	sat	8	0.5%	.999	comp	[Km90]
Mingshan; Tsinghua U.; PRC	s1	263-358	sat	--	--	.9998	4/90-->	
Kruse; U. Hannover; FRG	s1,sv	--	sat	--	--	--	9/89-8/91	
Diller; NIST; USA	l	175-320	sat-35	60	3%	--	comp	
Diller; NIST; USA	l,v	300-500	0.2-50	100	3%	--	10/90-10/91	
Snelson; NRC; Canada	s1	253-353	-	15	2.5-3.5%	-	3/91-10/91	

R134a; CH<sub>2</sub>FCF<sub>3</sub>; 1,1,1,2-tetrafluoroethane (continued)

Property Investigator	phase	range of data		no.	est.	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)	points	accuracy			
<b>Equation of State</b>								
Piao; Keio U.; Japan	l,v	300-425	0-12	-	-	-	comp	[Pi90]
Maurer; U. Kaiserlautern; FRG	l,v	210-500	0-12	-	-	-	comp	[Pl89]
Wakeham; Imperial Col., UK	l,v	--	--	-	-	-	planned	
Sengers; U. Maryland; USA	l,v	356-450	3-12	-	-	-	comp	[Sn90]
Ely; NIST; USA	l,v	170-450	0-70	-	-	-	3/90-12/90	[El90]
Oellrich; U. Karlsruhe; FRG	l,v	-	-	-	-	-	?/89-?/92	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90a]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gl90]
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

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R134a; CH<sub>2</sub>FCF<sub>3</sub>; 1,1,1,2-tetrafluoroethane (continued)

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R152a; CH<sub>3</sub>CHF<sub>2</sub>; 1,1-difluoroethane

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T(K)	p (MPa)					
<b>Vapor pressure</b>								
Baehr; U. Hannover; FRG	l-v	300-386	-	55	0.03%	.9995	7/89-6/91	
Blanke; PTB; FRG	l-v	156-386	-	18	0.1%	.9999	10/86-9/90	
Straub; T.U. München; FRG	l-v	330-386	-	50	0.5-1.5%	.9998	10/90-8/91	
Yin; Xi'an Jiaotong U.; PRC	l-v	242-293	-	21	1.5kPa	.9995	comp	[Yn90]
Kruse; U. Hannover; FRG	l-v	--	-	--	--	--	9/89-8/91	
Bier; U. Karlsruhe; FRG	l-v	203-386	-	--	0.1%	.998	comp	[Bi90]
Morrison; NIST; USA	l-v	268-383	-	10	-	.999	comp	
<b>Saturated liquid density</b>								
Baehr; U. Hannover; FRG	s1	293-383	-	10	0.1%	.9995	7/89-6/91	
Kruse; U. Hannover; FRG	s1	233-353	-	8	0.3%	--	comp	
Morrison; NIST; USA	s1	268-383	-	10	-	.999	comp	
<b>Pressure-volume-temperature</b>								
Baehr; U. Hannover; FRG	l,v	293-433	0.1-16	500	0.1%	.9995	7/89-6/91	
Blanke; PTB; FRG	l	156-470	sat-30	300	0.1%	.9999	10/86-9/90	
Straub; T.U. München; FRG	l,v	330-440	2-12	300	0.5-1.5%	.9998	10/90-8/91	
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	0.15%	.99	planned	
Kubota; Kobe U.; Japan	v	303-333	0.1-sat	30	3%	.9998	comp	
Kubota; Kobe U.; Japan	v	323-423	0.1-10	76	0.4%	.999	comp	
Majima; Keio U.; Japan	v	290-420	0.1-6	112	0.1%	.999	--	
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.999	comp	
<b>Virial coefficients</b>								
Schramm; Phys. Chem. Inst.;FRG	v	233-296	-	4	1%	--	comp	
<b>Critical parameters</b>								
Yin; Xi'an Jiaotong U.; PRC	T, $\rho$	-	-	-	15mK,0.5%	.9997	comp	[Yn90]
Bier; U. Karlsruhe; FRG	-	-	-	-	-	-	comp	[Bi90]
Schmidt; NIST; USA	T, $\rho$	-	-	--	0.01g/cm <sup>3</sup>	.9997	comp	[Ch90]
<b>Triple point temperature</b>								
Blanke; PTB; FRG	-	-	-	-	--	.9999	planned	
<b>Heat capacity/calorimetry</b>								
Nakagawa; Keio U.; Japan	l	--	--	--	0.4%	--	7/90-->	
Sami;U. Moncton; Canada	l,v	283-353	0.5-1.4	-	2%	--	in prog	
<b>Speed of sound</b>								
Kohler; Ruhr U.; FRG	v	230-350	0.02-0.5	400	0.01%	--	?/88-?/91	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	0.5%	--	4/90-->	
<b>Dielectric constant</b>								
Lehmann; U. Rostock; FRG	v	373-423	0.2-3	20	2%	.993	1/90-6/91	
Morrison; NIST; USA	v	298-433	0.04-0.6	-	3x10 <sup>-6</sup>	.999	comp	[My90]

R152a; CH<sub>3</sub>CHF<sub>2</sub>; 1,1-difluoroethane (continued)

Property Investigator	phase	range of data T(K)	p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Refractive index</b>								
Straub; T.U. München; FRG	l,v	330-440	2-12	300	0.05%	.9998	10/90-8/91	
Schmidt; NIST; USA	l,v	296-384	sat	40	0.001	.9997	comp	[Ch90]
<b>Surface Tension</b>								
Straub; T.U. München; FRG	l-v	230-386	-	100	0.5%	.9998	10/90-8/91	
Okada; Nagaoka U. Tech.; Japan	l-v	273-373	-	126	0.2mN/m	.9999	comp	[Ok90]
Schmidt; NIST; USA	l,v	296-384	-	29	0.15mN/m	.9997	comp	[Ch90]
<b>Thermal conductivity</b>								
Gross/Hahne; U. Stuttgart; FRG	l,v	260-360	--	--	1%	--	?/90-?/92	
Hemminger; PTB; FRG	v	303-463	0.1-0.1	7	2.5%	.997+	comp	[Hm89]
Yata; Kyoto Inst. Tech.; Japan	l	250-350	sat-30	--	--	--	planned	
<b>Thermal diffusivity</b>								
Fiebig; Ruhr U.; FRG	l	293-353	2-8	--	1%	.98	comp	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	1-2%	--	4/90-->	
Straub; T.U. München; FRG	l,v	330-440	2-12	300	0.5-1.5%	.9998	comp	
<b>Viscosity</b>								
Mayinger; T. U. München; FRG	v	300-425	0.1-7.5	--	0.5%	--	2/91-5/91	
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	2%	.99	planned	
Kumagai; Tohoku U.; Japan	s1	273-353	sat	8	0.5%	.999	comp	[Km90]
Kruse; U. Hannover; FRG	l	236-353	?-2.5	8	4%	.999	comp	
<b>Equation of State</b>								
Maurer; U. Kaiserlautern; FRG	l,v	164-470	0-50	-	-	-	comp	[Pl89]
Oellrich; U. Karlsruhe; FRG	l,v	-	-	-	-	-	?/89-?/92	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gl90]
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

## R152a; CH<sub>3</sub>CHF<sub>2</sub>; 1,1-difluoroethane (continued)

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**R134; CHF<sub>2</sub>CHF<sub>2</sub>; 1,1,2,2-tetrafluoroethane**

Property Investigator	phase	range of data T (K)	range of data p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Vapor pressure</b>								
Maezawa; Keio U.; Japan	l-v	200-390	-	38	10kPa	.994-.998	comp	[Mz90]
Tamatsu; Keio U.; Japan	l-v	303-390	-	34	3kPa	.9998	3/90-8/90	
Morrison; NIST; USA	l-v	268-383	-	10	-	.994	comp	
<b>Saturated liquid density</b>								
Fukushima; Asahi Glass Co.; Japan	s1	245-293	-	7	0.3%	.9994	comp	
Maezawa; Keio U.; Japan	s1	200-390	-	38	0.2%	.994-.998	comp	[Mz90]
Tatoh; Keio U.; Japan	s1	364-391	-	10	0.1%	.998-.999	4/90-->	
Morrison; NIST; USA	s1	268-383	-	10	-	.994	comp	
<b>Saturated vapor density</b>								
Tatoh; Keio U.; Japan	sv	388-391	-	9	0.5%	.998-.999	4/90-->	
<b>Pressure-volume-temperature</b>								
Vacek; Czech T.U.; Czech.	l	200-300	sat-55	--	0.1%	--	6/91-12/91	
Maezawa; Keio U.; Japan	l	280-320	sat-2	5	0.2%	.994-.998	comp	[Mz90]
Tamatsu; Keio U.; Japan	l,v	345-443	0.1-10	67	0.1%	.9998	3/90-8/90	
<b>Critical parameters</b>								
Tatoh; Keio U.; Japan	T, $\rho$	-	-	-	10mK,0.5%	.998-.999	4/90-->	
Schmidt; NIST; USA	T, $\rho$	-	-	--	0.01g/cm <sup>3</sup>	.994	comp	[Ch90]
<b>Dielectric constant</b>								
Morrison; NIST; USA	v	298-433	0.04-0.5	-	3x10 <sup>-6</sup>	.994	comp	[My90]
<b>Refractive index</b>								
Chae; Korea Std. Res. Lab.; Korea	l,v	230-456	0.1-5	--	1.0%	.99	planned	
Schmidt; NIST; USA	l,v	293-391	sat	22	0.001	.994	comp	[Ch90]
<b>Surface Tension</b>								
Chae; Korea Std. Res. Lab.; Korea	l-v	230-390	-	--	1.0%	.99	planned	
Schmidt; NIST; USA	l,v	293-391	-	17	0.15mN/m	.994	comp	[Ch90]
<b>Thermal conductivity</b>								
Chae; Korea Std. Res. Lab.; Korea	l,v	230-500	0.1-5	--	1.0%	.99	3/90-->	
<b>Equation of State</b>								
Morgenstern; HFV Dresden; FRG	l,v	220-480	0-4	-	-	-	comp	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gi90]
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

## R134; CHF<sub>2</sub>CHF<sub>2</sub>; 1,1,2,2-tetrafluoroethane (continued)

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**R124; CHClFCF<sub>3</sub>; 1-chloro-1,2,2,2-tetrafluoroethane**

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
<b>Vapor pressure</b>								
Fukushima; Asahi Glass Co.; Japan	l-v	--	-	--	5kPa	.9997	7/90-3/91	
Morrison; NIST; USA	l-v	273-373	-	25	-	.998	in prog	
<b>Saturated liquid density</b>								
Fukushima; Asahi Glass Co.; Japan	sl	250-310	-	8	0.3%	.9997	comp	
<b>Pressure-volume-temperature</b>								
Fukushima; Asahi Glass Co.; Japan	l,v	358-?	0.1-6	--	0.2%	.9997	7/90-3/91	
Sandarusi; NIST; USA	l,v	318-473	1.4-40	400	0.1-0.3%	.999+	planned	
<b>Critical parameters</b>								
Fukushima; Asahi Glass Co.; Japan	T,p	-	-	-	5mK,0.5%	.9997	6/90-12/90	
<b>Dielectric constant</b>								
Morrison; NIST; USA	v	298-433	0.04-0.4	-	3x10 <sup>-6</sup>	.998	comp	[My90]
<b>Thermal conductivity</b>								
Yata; Kyoto Inst. Tech.; Japan	l	250-350	sat-30	--	--	--	planned	
Perkins; NIST; USA	l,v	120-435	0.1-70	800	1%	--	1/91-9/92	
<b>Thermal diffusivity</b>								
Perkins; NIST; USA	l,v	120-435	0.1-70	800	5%	--	1/91-9/92	
<b>Viscosity</b>								
Snelson; NRC; Canada	sl	253-353	-	15	2.5-3.5%	-	3/91-10/91	
<b>Equation of State</b>								
Morgenstern; HFV Dresden; FRG	l,v	240-390	0-3.5	-	-	-	comp	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[E190]
Fischer; ORNL; USA	l,v	-	-	-	-	-	comp	[Fs90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp	[Gl90]
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

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**R142b; CCl<sub>2</sub>CH<sub>3</sub>; 1-chloro-1,1-difluoroethane**

Property Investigator	phase	range of data T (K)	range of data p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Vapor pressure</b>								
Blanke; PTB; FRG	l-v	142-410	-	18	0.1%	.9999	planned	
LeNeindre; U. Paris Nord; France	l-v	298-?	-	--	--	--	10/90-->	
Straub; T.U. München; FRG	l-v	--	-	50	--	.9998	10/90-8/91	
Fukushima; Asahi Glass Co.; Japan	l-v	335-410	-	--	5kPa	.9998	4/90-10/90	
Maezawa; Keio U.; Japan	l-v	320-400	-	12	10kPa	.998	comp	[Mz90]
Kumagai; Keio U.; Japan	l-v	297-410	-	69	3kPa	.998-.9998	comp	[Km90]
Bier; U. Karlsruhe; FRG	l-v	203-410	-	--	0.1%	.999	comp	[Bi90]
Morrison; NIST; USA	l-v	268-383	-	10	-	--	comp	
<b>Saturated liquid density</b>								
Fukushima; Asahi Glass Co.; Japan	s1	252-410	-	--	0.2%	.9998	4/90-10/90	
Maezawa; Keio U.; Japan	s1	210-400	-	36	0.2%	.998	comp	[Mz90]
Tanikawa; Keio U.; Japan	s1	353-410	-	9	0.1%	.999	comp	
Kumagai; Keio U.; Japan	s1	346-410	-	7	0.1%	.998-.9998	comp	[Km90]
Morrison; NIST; USA	s1	268-383	-	10	-	--	comp	
<b>Saturated vapor density</b>								
Tanikawa; Keio U.; Japan	sv	395-410	-	9	0.5%	.999	comp	
Kumagai; Keio U.; Japan	sv	357-410	-	7	0.1%	.998-.9998	comp	[Km90]
<b>Pressure-volume-temperature</b>								
Blanke; PTB; FRG	l	142-470	sat-30	300	0.1%	.9999	planned	
LeNeindre; U. Paris Nord; France	l	298-413	0.1-40	--	--	--	comp	
Nieto de Castro; U. Lisbon; Por	l	290-420	0-20	50	1%	.995	comp	[Cs90]
Straub; T.U. München; FRG	l,v	360-460	2-12	300	--	.9998	10/90-8/91	
Ström; Chalmers U. Tech.; Swe	l	258-323	0.5-2	--	0.15%	.99	planned	
Fukushima; Asahi Glass Co.; Japan	l,v	335- >T <sub>c</sub>	1-6	--	0.2%	.9998	4/90-10/90	
Maezawa; Keio U.; Japan	l	320-400	sat-2	6	0.2%	.998	comp	[Mz90]
Kumagai; Keio U.; Japan	l,v	345-443	0.3-9	70	0.1%	.998-.9998	comp	[Km90]
<b>Virial coefficients</b>								
Schramm; Phys.-Chem. Inst.; FRG	v	248-296	--	4	1%	--	comp	
<b>Critical parameters</b>								
LeNeindre; U. Paris Nord; France	--	-	-	--	--	--	10/90-->	
Fukushima; Asahi Glass Co.; Japan	T,p	-	-	--	10mK,0.1%	.9998	10/89-8/90	
Tanikawa; Keio U.; Japan	T,p	-	-	--	10mK,0.5%	.999	comp	
Bier; U. Karlsruhe; FRG	-	-	-	-	-	.999	comp	[Bi90]
Schmidt; NIST; USA	T,p	-	-	--	0.01g/cm <sup>3</sup>	.9997	comp	[Ch90]
<b>Triple point temperature</b>								
Blanke; PTB; FRG	-	-	-	-	--	.9999	planned	
<b>Heat capacity/calorimetry</b>								
Nakagawa; Keio U.; Japan	l	276-340	1-3	19	0.4%	--	5/90-->	

R142b;  $\text{CClF}_2\text{CH}_3$ ; 1-chloro-1,1-difluoroethane (continued)

Property	Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
			T(K)	p (MPa)					
<b>Speed of sound</b>									
Kohler; Ruhr U.; FRG		v	230-350	0.025-0.5	400	0.01%	.999	?/88-?/91	
Leipertz; U. Erlangen-Nürnberg; FRG		l,v	240-450	<15	--	0.5%	--	4/90-->	
LeNeindre; U. Paris Nord; France		l	298-523	0.1-100	--	--	--	10/90-->	
Trusler; Imperial Col.; UK		v	--	0-4	50	0.005%	--	10/90-->	
<b>Dielectric constant</b>									
Nieto de Castro; U. Lisbon; Por		l,v	--	0-20	--	0.5%	.995	12/89-10/93	
<b>Refractive index</b>									
Straub; T.U. München; FRG		l,v	360-460	-	300	0.05%	.9998	10/90-8/91	
Schmidt; NIST; USA		l,v	296-409	sat	36	0.001	.9997	comp	[Ch90]
<b>Surface Tension</b>									
Straub; T.U. München; FRG		l-v	230-410	-	100	0.5%	.9998	10/90-8/91	
Schmidt; NIST; USA		l,v	296-409	-	39	0.15mN/m	.9997	comp	[Ch90]
<b>Thermal conductivity</b>									
LeNeindre; U. Paris Nord; France		l	298-523	0.1-70	--	1-2%	--	comp	
Nieto de Castro; U. Lisbon; Por		l,v	290-504	0-20	50	2%	.995	comp	[Cs90]
Stephan/Taxis; U. Stuggart; FRG		v	273-423	<5	100	1%	--	-->9/91	
Yata; Kyoto Inst. Tech.; Japan		l	250-350	sat-30	100	--	--	planned	
Tanaka; Kobe U.; Japan		v	293-353	0.1-sat	21	2%	.999	comp	[Tn90]
Perkins; NIST; USA		l,v	160-450	0.1-70	800	1%	--	-->12/90	
Venart; U. New Brunswick; Canada		l,v	203-393	0.1-70	--	1%	--	planned	
<b>Thermal diffusivity</b>									
Fiebig; Ruhr U.; FRG		l	293-353	2-8	--	--	.99	comp	
Leipertz; U. Erlangen-Nürnberg; FRG		l,v	240-450	<15	--	1-2%	--	4/90-->	
Straub; T.U. München; FRG		l,v	360-460	2-12	300	1-2%	.9998	10/90-8/91	
Perkins; NIST; USA		l,v	160-450	0.1-70	800	5%	--	-->12/90	
Venart; U. New Brunswick; Canada		l,v	203-393	0.1-70	--	5%	--	planned	
<b>Viscosity</b>									
Mayinger; T. U. München; FRG		v	300-384	0.1-2	28	0.5%	.9991	comp	[My90]
Ström; Chalmers U. Tech.; Swe		l	258-323	0.5-2	--	2%	.99	planned	
Kruse; U. Hannover; FRG		l	236-353	?-2.5	8	4%	.999	comp	
<b>Equation of State</b>									
Maurer; U. Kaiserlautern; FRG		v	257-427	0-4	-	-	-	comp	[Pl90]
Oellrich; U. Karlsruhe; FRG		l,v	-	-	-	-	-	?/89-?/92	
Huber; NIST; USA		l,v	all	all	-	-	-	in prog	[E190]
Gallagher; NIST; USA		l,v	0.5-1.6 $T_c$	0-2 $P_c$	-	-	-	comp	[Gl90]
<b>Ideal Gas Properties</b>									
Lucas; U. Duisburg; FRG		-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA		-	0-1500	0.1	-	--	-	comp	[TR90]

## R142b; $\text{CClF}_2\text{CH}_3$ ; 1-chloro-1,1-difluoroethane (continued)

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R123; CHCl<sub>2</sub>CF<sub>3</sub>; 1,1-dichloro-2,2,2-trifluoroethane

Property Investigator	phase	range of data T (K)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Vapor pressure</b>							
Baroncini; U. Ancona; Italy	l-v	240-360	-	--	0.5%	--	7/90-6-91
Gorenflo; U. Paderborn; FRG	l-v	293-423	-	27	0.04%	.95-.97	--
LeNeindre; U. Paris Nord; France	l-v	298-?	-	--	--	--	10/90-->
Straub; T.U. München; FRG	l-v	360-460	-	50	0.5-1.5%	.998	7/90-12/90
Oguchi; Kanagawa Inst. Tech.; Japan	l-v	243-456	-	45	0.5kPa	.998	comp
Kubota; Kobe U.; Japan	l-v	273-457	-	38	3kPa	.995	comp
Fukushima; Asahi Glass Co.; Japan	l-v	314-456	-	65	5kPa	.998-.999	comp
Maezawa; Keio U.; Japan	l-v	280-350	-	8	7kPa	.9993	comp
Piao; Keio U.; Japan	l-v	310-456	-	67	2kPa	.998-.9993	?/89-?/91
Qian; Keio U.; Japan	l-v	310-420	-	36	1kPa	.996-.9994	5/90-7/90
Mingshan; Tsinghua U.; PRC	l-v	248-358	-	20	0.02%	--	planned
Magee; NIST; USA	l-v	166-400	-	--	0.01-0.05%	.9999	5/91-9/91
Weber; NIST; USA	l-v	273-457	-	64	0.05%	.9995	comp
Morrison; NIST; USA	l-v	268-383	-	15	-	.9999	comp
Morrison; NIST; USA	l-v	273-373	-	25	-	.9999	in prog
<b>Saturated liquid density</b>							
Gorenflo; U. Paderborn; FRG	s1	295-423	-	27	0.04%	.95-.97	--
Yokoyama; Tohoku U.; Japan	s1	248-423	-	24	0.2-0.3%	.996-.999	comp
Oguchi; Kanagawa Inst. Tech.; Japan	s1	254-433	-	17	0.1%	.998	comp
Fukushima; Asahi Glass Co.; Japan	s1	281-456	-	35	0.3%	.998-.999	comp
Maezawa; Keio U.; Japan	s1	200-400	-	23	0.2%	.9993	comp
Piao; Keio U.; Japan	s1	300-420	-	5	0.15%	.998-.9993	?/89-?/91
Tanikawa; Keio U.; Japan	s1	401-456	-	10	0.1-0.5%	.998-.9999	comp
Weber; NIST; USA	s1	300-457	-	-	0.05%	.9995	comp
Morrison; NIST; USA	s1	268-383	-	10	-	.9999	comp
<b>Saturated vapor density</b>							
Gorenflo; U. Paderborn; FRG	sv	293-423	-	27	0.2%	.95-.97	--
Fukushima; Asahi Glass Co.; Japan	sv	352-456	-	27	0.3%	.998-.999	comp
Tanikawa; Keio U.; Japan	sv	438-456	-	9	0.1-0.5%	.998-.9999	comp
Weber; NIST; USA	sv	433-457	-	5	0.05%	.9995	comp

R 123; CHCl<sub>2</sub>CF<sub>3</sub>; 1,1-dichloro-2,2,2-trifluoroethane (continued)

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
<b>Pressure-volume-temperature</b>								
Baroncini; U. Ancona; Italy	v	240-360	0.1-sat	--	0.5%	--	7/90-6-91	
LeNeindre; U. Paris Nord; France	l,v	298-413	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.3%	.995	12/89-10/93	
Straub; T.U. München; FRG	l,v	360-460	0.7-12	300	0.5-1.5%	.998	7/90-12/90	
Oguchi; Kanagawa Inst. Tech.; Japan	l	243-493	0.07-16	27	0.01%	.998	comp	
Matsuo; Kobe U.; Japan	l	293-323	sat-40	68	0.04%	.999	comp	[Ko90]
Matsuo; Kobe U.; Japan	l	293-353	sat-40	44	0.02%	.999	comp	[Ko88]
Fukushima; Asahi Glass Co.; Japan	l,v	352-484	1-5	59	0.2%	.998-.999	comp	
Maezawa; Keio U.; Japan	l	280-340	sat-2	16	0.2%	.9993	comp	[Mz90]
Piao; Keio U.; Japan	l,v	310-525	0.5-12	134	0.15%	.998-.9993	?/89-?/91	
Qian; Keio U.; Japan	v	310-420	0.1-sat	65	0.2-0.7%	.996-.9994	5/90-7/90	
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->	
Mingshan; Tsinghua U.; PRC	v	248-358	0.1-6	80	0.2%	--	planned	
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.9999	comp	
Weber; NIST; USA	v	338-453	0-sat	75	0.05%	.9995	comp	[Wb90]
<b>Virial coefficients</b>								
Schramm; Phys.-Chem. Inst.; FRG	v	268-296	--	2	5%	--	comp	
<b>Critical parameters</b>								
LeNeindre; U. Paris Nord; France	--	-	-	--	--	--	10/90-->	
Straub; T.U. München; FRG	--	-	-	--	0.5-1.5%	.998	7/90-12/90	
Kubota; Kobe U.; Japan	T,P	-	-	50mK,3kPa	.995	comp	[Kb89]	
Fukushima; Asahi Glass Co.; Japan	T,p	-	-	25mK	.998-.999	comp		
Piao; Keio U.; Japan	P	-	-	2kPa	.998-.9993	?/89-?/91		
Tanikawa; Keio U.; Japan	T,p	-	-	10mK,0.5%	.998-.9999	comp		
Weber; NIST; USA	T,P,p	-	-	0.05%	.9995	comp	[Wb90]	
<b>Heat capacity/calorimetry</b>								
Nakagawa; Keio U.; Japan	l	276-440	sat-3	80	0.4%	.9982	comp	
Magee; NIST; USA	l	166-340	sat-35	--	0.5%	.9999	5/91-9/91	
<b>Speed of sound</b>								
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	0.5%	--	4/90-->	
LeNeindre; U. Paris Nord; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Trusler; Imperial Col.; UK	v	--	0-4	50	0.005%	--	10/90-->	
Takagi; Kyoto Inst. Tech.; Japan	l	280-370	sat-75	170	0.2%	.998	comp	
Mingshan; Tsinghua U.; PRC	v	248-358	0.1-1.5	--	0.2%	--	planned	
Goodwin; NIST; USA	v	260-335	0.02-0.07	49	0.01%	.9995	in prog	
<b>Dielectric constant</b>								
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.5%	.995	12/89-10/93	
Tanaka; Kobe U.; Japan	l	298-313	sat-35	32	1%	.999	--	[Ko90]
Morrison; NIST; USA	v	298-433	0.04-0.1	-	3x10 <sup>-6</sup>	.9999	comp	[Me90]

R123; CHCl<sub>2</sub>CF<sub>3</sub>; 1,1-dichloro-2,2,2-trifluoroethane (continued)

Property Investigator	phase	range of data T(K)	p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Refractive index</b>								
Straub; T.U. München; FRG	l,v	360-460	0.7-12	300	0.05%	.998	7/90-12/90	
Chae; Korea Std. Res. Lab.; Korea	l,v	230-456	0.1-5	--	1.0%	.99	planned	
<b>Surface Tension</b>								
Straub; T.U. München; FRG	l-v	223-457	-	100	0.5%	.998	planned	
Higashi; Iwaki Meisei U.; Japan	l-v	273-290	-	21	0.4mN/m	.9984	in prog	
Okada; Nagaoka U. Tech.; Japan	l-v	237-443		186	0.2mN/m	.9984	comp	[Ok90]
Chae; Korea Std. Res. Lab.; Korea	l-v	230-456	-	--	1.0%	.99	planned	
Mingshan; Tsinghua U.; PRC	l-v	263-358	-	--	--	--	planned	
Schmidt; NIST; USA	l-v	253-423	-	22	0.15mN/m	.995	comp	[Ch90]
<b>Thermal conductivity</b>								
Assael; Aristotle U.; Greece	l,v	230-370	<40	--	0.5%	--	6/89-?	
Gross/Hahne; U. Stuggart; FRG	l,v	260-364	0.1-8.0	65	1%	.995	?/88-?/92	[Gr90]
LeNeindre; U. Paris Nord; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.5%	.995	12/89-10/93	
Yata; Kyoto Inst. Tech.; Japan	l	250-350	sat-30	127	--	.995-.9995	comp	[Yt89]
Tanaka; Kobe U.; Japan	l	283-323	sat-200	36	1.0%	.999	comp	[Tn88]
Matsuo; Kobe U.; Japan	l	298-323	sat-100	33	1%	.999	in prog	
Nagasaki; Keio U.; Japan	l	273-353	sat-40	--	0.5%	.998	?/89-->	
Chae; Korea Std. Res. Lab.; Korea	l,v	230-500	0.1-5	--	1.0%	.99	3/90-->	
Perkins; NIST; USA	l,v	180-450	0.1-70	800	1%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	1%	--	in prog	
<b>Thermal diffusivity</b>								
Fiebig; Ruhr U.; FRG	l	273-363	1-8	--	1%	--	8/90-12/90	
Leipertz; U. Erlangen-Nürnberg; FRG	l,v	240-450	<15	--	1-2%	--	4/90-->	
Straub; T.U. München; FRG	l,v	360-460	0.7-12	300	0.5-1.5%	.998	7/90-12/90	
Perkins; NIST; USA	l,v	180-450	0.1-70	800	5%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	5%	--	in prog	
<b>Viscosity</b>								
Matthews; Polytech. S.W.; UK	v	301-573	0.01-0.1	10	0.5%	--	1/90-->	
Mayinger; T.U. München; FRG	v	300-425	0.1-2.1	28	0.5%	.999	comp	[My90]
Takahashi; Tohoku U.; Japan	v	323-423	0.1-sat	48	0.3%	.996	comp	[Tk90]
Kumagai; Tohoku U.; Japan	s1	273-353	sat	9	0.5%	.996	comp	[Km90]
Tanaka; Kobe U.; Japan	l	293-313	sat-100	12	2%	.999	--	
Nagashima; Keio U.; Japan	l	233-418	sat-20	--	--	.9977	?/89-->	
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->	
Mingshan; Tsinghua U.; PRC	s1	263-358	-	--	--	--	planned	
Diller; NIST; USA	l	170-320	sat-35	60	3%	--	comp	
Snelson; NRC; Canada	s1	253-353	-	15	2.5-3.5%	-	3/91-10/91	

R123; CHCl<sub>2</sub>CF<sub>3</sub>; 1,1-dichloro-2,2,2-trifluoroethane (continued)

Property Investigator	phase	range of data T(K)      p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
Equation of State							
Maurer; U. Kaiserlautern; FRG	v	288-368	0-0.7	-	-	-	--
Huber; NIST; USA	l,v	all	all	-	-	-	in prog [El90]
Gallagher; NIST; USA	l,v	0.5-1.6 T <sub>c</sub>	0-2 P <sub>c</sub>	-	-	-	comp [Gl90]
Ideal Gas Properties							
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp [TR90]

Notes and References

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R123a; CHClFCClF<sub>2</sub>; 1,2-dichloro-1,2,2-trifluoroethane

Property Investigator	phase	range of data T(K)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
		p (MPa)					
Vapor pressure							
Otake; Tohoku U.; Japan	l-v	297-447	-	20	0.1kPa	.998	comp [Ot89]
Kubota; Kobe U.; Japan	l-v	303-458	-	32	3kPa	.998	comp [Kb89]
Morrison; NIST; USA	l-v	268-383	-	10	-	.991	comp
Saturated liquid density							
Yokoyama; Tohoku U.; Japan	s1	247-422	-	31	0.3%	.998-.999	comp [Yk88]
Morrison; NIST; USA	s1	268-383	-	10	-	.991	comp
Pressure-volume-temperature							
Otake; Tohoku U.; Japan	v	374-465	0.5-5	19	0.5%	.998	comp [Ot89]
Matsuo; Kobe U.; Japan	l	293-333	sat-40	44	0.04%	.999	comp [Ko89a]
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.991	comp
Critical parameters							
Schmidt; NIST; USA	T,p	-	-	--	0.01g/cm <sup>3</sup>	.991	comp [Ch90]
Speed of sound							
Goodwin; NIST; USA	v	260-300	0.004-0.06	18	0.01%	-	in prog
Dielectric constant							
Morrison; NIST; USA	v	298-433	0.04-0.1	-	3x10 <sup>-6</sup>	.991	comp [My90]
Refractive index							
Schmidt; NIST; USA	l,v	297-460	sat	40	0.001	.991	comp [Ch90]
Surface tension							
Schmidt; NIST; USA	l,v	297-460	sat	29	0.15mN/m	.991	comp [Ch90]
Thermal conductivity							
Hemminger; PTB; FRG	v	303-463	0.1-0.1	7	2.5%	.997	comp [Hm89]
Viscosity							
Takahashi; Tohoku U.; Japan	v	323-423	0.1-sat	47	0.3%	--	comp [Tk90]
Kumagai; Tohoku U.; Japan	s1	273-353	sat	9	0.5%	.998	comp [Km90]
Tanaka; Kobe U.; Japan	l	298-323	sat-120	39	2%	.999	comp [Ko89]
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->
Ideal Gas Properties							
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp [TR90]

## R123a; CHClFCClF<sub>2</sub>; 1,2-dichloro-1,2,2-trifluoroethane (continued)

### Notes and References

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R141b; CCl<sub>2</sub>FCH<sub>3</sub>; 1,1-dichloro-1-fluoroethane

Property Investigator	phase	range of data T (K)	range of data p (MPa)	no. points	est. accuracy	sample purity	start/end dates	note /ref.
<b>Vapor pressure</b>								
LeNeindre; U. Paris Nord; France	l-v	298-480	-	--	--	--	10/90-->	
Kubota; Kobe U.; Japan	l-v	278-373	-	24	3kPa	.999	comp	
Maezawa; Keio U.; Japan	l-v	200-400	-	37	10kPa	.988	comp	[Mz90]
Holste; Texas A&M U.; USA	l-v	250-400	-	--	0.1%	--	9/90-10/91	
Weber; NIST; USA	l-v	273-418	-	39	0.05%	.9994	comp	
Morrison; NIST; USA	l-v	268-383	-	10	-	.9994	comp	
<b>Saturated liquid density</b>								
Kumagai; Tohoku U.; Japan	s1	273-353	-	9	0.2%	.995	comp	[Km90]
Fukushima; Asahi Glass Co.; Japan	s1	245-369	-	--	0.3%	.9947	comp	
Maezawa; Keio U.; Japan	s1	200-400	-	37	0.2%	.988	comp	[Mz90]
Holste; Texas A&M U.; USA	s1	250-400	-	--	0.1%	--	9/90-10/91	
Morrison; NIST; USA	s1	268-383	-	10	-	.9994	comp	
Morrison; NIST; USA	s1	273-373	-	25	-	.9994	in prog	
<b>Saturated vapor density</b>								
Holste; Texas A&M U.; USA	sv	250-400	-	--	0.1%	--	9/90-10/91	
<b>Pressure-volume-temperature</b>								
LeNeindre; U. Paris Nord; France	l,v	298-413	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.3%	.995	12/89-10/93	
Matsuo; Kobe U.; Japan	l	293-348	sat-100	111	0.05%	.999	comp	[Ko90]
Kubota; Kobe U.; Japan	l,v	298-323	0.1-200	63	0.1-0.3%	.999	?/89-->	
Maezawa; Keio U.; Japan	l	280-400	sat-2	24	0.2%	.988	comp	[Mz90]
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->	
Holste; Texas A&M U.; USA	l,v	250-400	0-70	--	0.1%	--	9/90-10/91	
Weber; NIST; USA	v	329-418	0-sat	50	0.05%	.9994	comp	
Morrison; NIST; USA	l	268-378	sat-7	60	0.1%	.9994	comp	
<b>Critical parameters</b>								
LeNeindre; U. Paris Nord; France	-	-	-	--	--	--	10/90-->	
Holste; Texas A&M U.; USA	T,P, $\rho$	-	-	--	0.1%	--	9/90-10/91	
Schmidt; NIST; USA	T, $\rho$	-	-	--	0.01g/cm <sup>3</sup>	.9995	comp	[Ch90]
<b>Speed of sound</b>								
LeNeindre; U. Paris Nord; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Trusler; Imperial Col.; UK	v	--	0-4	50	0.005%	--	10/90-->	
Goodwin; NIST; USA	v	260-315	0.004-0.05	45	0.01%	.9994	in prog	
<b>Dielectric constant</b>								
Nieto de Castro; U. Lisbon; Por.	l,v	<T <sub>c</sub>	<20	--	0.5%	.995	12/89-10/93	
Morrison; NIST; USA	v	298-433	0.04-0.1	-	3x10 <sup>-6</sup>	.9994	comp	[My90]
<b>Refractive index</b>								
Schmidt; NIST; USA	l,v	323-476	sat	40	0.001	.9995	comp	[Ch90]

R141b;  $\text{CCl}_2\text{FCH}_3$ ; 1,1-dichloro-1-fluoroethane (continued)

Property Investigator	phase	range of data		no. points	est. accuracy	sample purity	start/end dates	note /ref.
		T (K)	p (MPa)					
<b>Surface tension</b>								
Schmidt; NIST; USA	l,v	323-476	-	28	0.15mN/m	.9995	comp	[Ch90]
<b>Thermal conductivity</b>								
LeNeindre; U. Paris Nord; France	l,v	298-523	0.1-100	--	--	--	10/90-->	
Nieto de Castro; U. Lisbon; Por.	l,v	< $T_c$	<20	--	0.5%	.995	12/89-10/93	
Wakeham; Imperial Col.; UK	s1,sv	260-370	sat	20	--	.999	comp	[Wk90]
Yata; Kyoto Inst. Tech.; Japan	l	250-350	sat-30	--	--	.995-.9995	--	
Tanaka; Kobe U.; Japan	v	293-353	0.1-0.1	4	2%	.999	comp	[Tn90]
Matsuo; Kobe U.; Japan	l	298-313	sat-60	13	1%	.999	in prog	
Perkins; NIST; USA	l,v	180-450	0.1-70	800	1%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	1%	--	planned	
<b>Thermal diffusivity</b>								
Perkins; NIST; USA	l,v	180-450	0.1-70	800	5%	--	1/91-9/92	
Venart; U. New Brunswick; Canada	l,v	203-393	0.1-70	--	5%	--	planned	
<b>Viscosity</b>								
Kumagai; Tohoku U.; Japan	s1	273-353	sat	9	0.5%	.995	comp	[Km90]
Tanaka; Kobe U.; Japan	l	298-323	sat-120	39	2%	.999	comp	
Woolf; Australian Nat. U.; Aus.	l	273-338	sat-400	--	0.1-0.5%	--	8/90-->	
Diller; NIST; USA	l	180-320	sat-35	60	3%	--	comp	
<b>Equation of State</b>								
Morgenstern; HFV Dresden; FRG	l,v	273-520	0-4	-	-	-	comp	
Huber; NIST; USA	l,v	all	all	-	-	-	in prog	[El90]
<b>Ideal Gas Properties</b>								
Lucas; U. Duisburg; FRG	-	100-500	0-0	-	1%	-	in prog	
Marsh; Texas A&M; USA	-	0-1500	0.1	-	--	-	comp	[TR90]

Notes and References

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## Other Pure Fluids

Fluid/Investigator/ /Property	phase	range of data		no.	est.	sample	start/end	note /ref.
		T (K)	p (MPa)	points	accuracy	purity	dates	
R227								
Gorenflo; U. Paderborn; FRG								
vapor pressure	l-v	293-375	-	17	0.04%	.995	in prog	
sat. liquid density	s1	293-370	-	17	0.04%	.995	in prog	
sat. vapor density	sv	293-370	-	17	0.2%	.995	in prog	
R124a								
Morgenstern; HFV Dresden; FRG								
equation of state	l,v	243-450	0-3.5	-	-	-	comp	[Mr90]
R225ca								
Widiatmo; Keio U.; Japan								
vapor pressure	l-v	T <sub>bp</sub> -400	-	--	10kPa	--	7/90-3/91	
saturation density	s1	T <sub>bp</sub> -400	-	--	0.2%	--	7/90-3/91	
pressure-volume-temperature	l	280-400	sat-2	--	0.2%	--	7/90-3/91	
Higashi; Iwaki Meisei U.; Japan								
surface tension	l-v	273-320	-	--	0.2mN/m	--	in prog	
bis-difluoromethylether								
Gillis; NIST; USA								
sound speed	v	255-330	0.01-.2	-	0.01%	.998	in prog	
Schmidt; NIST; USA								
critical parameters	T, $\rho$	-	-	-	0.01g/cm <sup>3</sup>	-	in prog	
density	s1	T <sub>nbp</sub> -T <sub>c</sub>	sat	41	-	-	in prog	
refractive index	s1,sv	T <sub>nbp</sub> -T <sub>c</sub>	sat	41	0.001	-	in prog	
surface tension	l-v	T <sub>nbp</sub> -T <sub>c</sub>	-	74	0.15mN/m	-	in prog	
2-, 3-, and 4-carbon fluoro- and hydrofluoroethers								
Adcock; U. Tennessee; USA								
vapor pressure	l-v	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.9998	8/88-2/92	[Ad90]
saturation density	s1	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.9998	8/88-2/92	[Ad90]
pressure-volume-temperature	--	--	--	6	2%	.9998	8/88-2/92	[Ad90]
critical parameters	--	-	-	--	--	.9998	8/88-2/92	[Ad90]
heat capacity	--	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.9998	8/88-2/92	[Ad90]
viscosity	s1	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.9998	8/88-2/92	[Ad90]
3- and 4-carbon hydrofluorocarbons and hydrochlorofluorocarbons								
DesMarteau; Clemson U.; USA								
vapor pressure	l-v	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.98+	8/88-8/91	[Hw90]
saturation density	s1	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.98+	8/88-8/91	[Hw90]
pressure-volume-temperature	--	--	--	6	2%	.98+	8/88-8/91	[Hw90]
critical parameters	--	-	-	--	--	.98+	8/88-8/91	[Hw90]
heat capacity	--	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.98+	8/88-8/91	[Hw90]
viscosity	s1	T <sub>nbp</sub> -T <sub>c</sub>	-	--	2%	.98+	8/88-8/91	[Hw90]

## Other Pure Fluids (continued)

### Notes and References

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## Mixture Studies

Mixture/Investigator/ Property	phase	T(K)	range of data p (MPa)	x	no. points	est. accuracy	start/end dates	note /ref.
R14/23 Maurer; U. Kaiserlautern; FRG equation of state	l,v	203-473	0-58	--	-	-	comp	[Pl90]
R23/13 Maurer; U. Kaiserlautern; FRG equation of state	l,v	203-473	0-58	--	-	-	comp	[Pl90]
R23/22 Morrison; NIST; USA bubble point pressure	l-v	268-T <sub>c</sub>	-	50	10	-	comp	
R23/142b Morrison; NIST; USA bubble point pressure	l-v	268-T <sub>c</sub>	-	50	10	-	comp	
R32/134a Holste; Texas A&M U.; USA vapor-liquid equilibria P-V-T-x	l-v	175-T <sub>c</sub>	-	50	--	0.1%	6/91-12/91	
	l,v	175-400	0-70	50	--	0.1%	6/91-12/91	
R32/152a Holste; Texas A&M U.; USA vapor-liquid equilibria P-V-T-x	l-v	175-T <sub>c</sub>	-	50	--	0.1%	1/92-6/92	
	l,v	175-400	0-70	50	--	0.1%	1/92-6/92	
R125/134a Snellson; NRC; Canada viscosity	s1	253-353	-	0-100	50	2.5-3.5%	3/91-10/91	
R125/124 Snellson; NRC; Canada viscosity	s1	253-353	-	0-100	50	2.5-3.5%	3/91-10/91	
R143a/22 Tanaka; Kobe U.; Japan viscosity	v	293-313	0.1-0.1	0-100	15	1%	comp	[Ko90]
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	273-338	-	--	114	1.5%	comp	
R22/12 Takahashi; Tohoku U.; Japan viscosity	v	298-398	0.1-6	43-79	207	0.3%	comp	[Tk89]

## Mixture Studies (continued)

Mixture/Investigator/ Property	phase	T (K)	range of data		x	no. points	est. accuracy	start/end dates	note /ref.
<b>R22/134a</b>									
Tanaka; Kobe U.; Japan viscosity	v	293-313	0.1-0.1	0-100		15	1%	comp	[Ko90]
Yoshida; Matsushita Elec.; Japan vapor-liquid equilibria	l-v	273-323	-	--	--		0.4mol%	comp	
<b>R22/152a</b>									
Kruse; U. Hannover; FRG viscosity	l	243-353	?-2.5	0-100	--		4%	comp	
saturated liquid density	sl	233-353	--	0-100	76		0.3%	comp	
Mayinger; T. U. München; FRG viscosity	v	300-425	0.1-6.5	25-75	--		0.5%	7/91-10/91	
Schramm; Phys. Chem. Inst.; FRG second virial coefficient	v	233-296	-	--	4		2%	comp	
Ström; Chalmers U. Tech.; Swe vapor-liquid equilibria	l-v	--	0.1-2	--	--		0.3mol%	comp	
P-V-T-x	l	258-323	0.5-2	--	--		0.15%	comp	
heat capacity	l	253-313	sat-2	--	--		0.5%	in prog	
viscosity	l	258-323	0.5-2	--	--		2%	comp	
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	263-323	-	--	114		1.7%	comp	
P-V-T-x	v	348-423	0.1-4	30-70	26		0.4%	comp	
Maezawa; Keio U.; Japan bubble point pressure	l-v	280-380	-	10-90	66		20kPa	comp	[Mz90c]
saturated liquid density	sl	280-380	-	10-90	66		0.3%	comp	[Mz90c]
vapor-liquid equilibria	l-v	280-380	-	10-90	66		0.1%	comp	[Mz90c]
Wang; Xi'an Jiaotong U.; PRC saturation density	sl,sv	323-T <sub>c</sub>	--	0-100	210		0.5%	comp	
Canren; Tianjin U.; PRC equation of state	v	--	--	--	-		-	--	
Bier; U. Karlsruhe; FRG critical parameters	T,P, $\rho$	-	-	0-100	-		0.05K; 6kPa	comp	[Bi90]
Oellrich; U. Karlsruhe; FRG equation of state	l,v	-	-	-	-		-	?/89-?/92	
Sami; U. Moncton; Canada heat capacity	l,v	283-353	0.5-1.4	-	-		2%	in prog	
LaRue; CRIQ; Canada bubble point pressure	l-v	.65-.85 T <sub>c</sub>	-	0-100	-		1%	comp	[Lr90]
<b>R22/152a/142b</b>									
Maezawa; Keio U.; Japan bubble point pressure	l-v	280-390	-	(6 comp)	71		20kPa	comp	[Mz90]
saturated liquid density	sl	280-390	-	(6 comp)	71		0.2%	comp	[Mz90]
vapor-liquid equilibria	l-v	280-390	-	(6 comp)	71		0.2%	comp	[Mz90]
<b>R22/152a/114</b>									
Sami; U. Moncton; Canada heat capacity	l,v	283-353	0.5-1.4	-	-		2%	in prog	

### Mixture Studies (continued)

Mixture/Investigator/ /Property	phase	T (K)	range of data p (MPa)	x	no. points	est. accuracy	start/end dates	note /ref.
R22/142b								
Kruse; U. Hannover; FRG viscosity	l	237-353	?-2.5	0-100	72	4%	comp	
LeNeindre; U. Paris Nord; France vapor pressure	l-v	298-?	-	40/60	--	--	10/90-->	
P-V-T-x	l,v	298-413	0.1-100	40/60	--	--	10/90-->	
critical parameters	-	-	-	40/60	--	--	10/90-->	
sound speed	l,v	298-523	0.1-100	40/60	--	--	10/90-->	
thermal conductivity	l,v	298-523	0.1-100	40/60	--	--	10/90-->	
Mayinger; T. U. München; FRG viscosity	v	300-425	0.1-6.5	25-75	--	0.5%	9/90-12/90	
Schramm; Phys. Chem. Inst.; FRG second virial coefficient	v	248-296	-	--	4	1%	comp	
Stephan/Taxis; U. Stuttgart; FRG thermal conductivity	v	273-423	?-5	--	100	1%	-->9/91	
Ström; Chalmers U. Tech.; Swe vapor-liquid equilibria	l-v	--	0.1-2	--	--	0.3mol%	comp	
P-V-T-x	l	258-323	0.5-2	--	--	0.15%	comp	
heat capacity	l	253-313	sat-2	--	--	0.5%	in prog	
viscosity	l	258-323	0.5-2	--	--	2%	comp	
Tanaka; Kobe U.; Japan viscosity	v	298-323	0.1-0.1	0-100	11	1%	comp	[Ko89]
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	263-338	-	--	174	1.5%	comp	
Yoshida; Matsushita Elec.; Japan vapor-liquid equilibria	l-v	273-323	-	--	--	0.4mol%	comp	
Maezawa; Keio U.; Japan bubble point pressure	l-v	280-400	-	20-80	46	20kPa	comp	[Mz90b]
saturated liquid density	s1	280-400	-	20-80	46	0.2%	comp	[Mz90b]
vapor-liquid equilibria	l-v	280-400	-	20-80	46	0.1%	comp	[Mz90b]
Kumagai; Keio U.; Japan vapor-liquid equilibria	l-v	321-T <sub>c</sub>	-	20-80	31	0.1%	comp	[Km90]
P-V-T-x	l,v	297-443	0.5-10	20-80	445	0.1%	comp	[Km90]
Yujun; Zhejiang U.; PRC vapor-liquid equilibria	l-v	243-373	-	0-100	--	0.5mol%	5/90-9/90	
Canren; Tianjin U.; PRC equation of state	v	--	--	--	-	-	--	
Bier; U. Karlsruhe; FRG critical parameters	T,P,p	-	-	0-100	-	0.05K; 6kPa	comp	[Bi90]
Oellrich; U. Karlsruhe; FRG equation of state	l,v	-	-	-	-	-	?/89-?/92	
LaRue; CRIQ; Canada bubble point pressure	l-v	.65-.85 T <sub>c</sub>	-	0-100	-	1%	comp	[Lr90]
Morrison; NIST; USA bubble point pressure	l-v	268-383	-	50	10	-	comp	

## Mixture Studies (continued)

Mixture/Investigator/ Property	phase	T(K)	range of data p (MPa)	x	no. points	est. accuracy	start/end dates	note /ref.
R22/152a/124 Yujun; Zhejiang U.; PRC vapor-liquid equilibria	l-v	243-373	-	0-100	--	0.5 mol%	2/91-7/91	
R22/114 Mayinger; T. U. München; FRG viscosity	v	300-425	0.1-5.3	25-75	--	0.5%	comp	[Nb90]
Ström; Chalmers U. Tech.; Swe vapor-liquid equilibria	l-v	--	0.1-2	--	--	0.3 mol%	comp	
P-V-T-x	l	258-323	0.5-2	--	--	0.15%	comp	
heat capacity	l	253-313	sat-2	--	--	0.5%	in prog	
viscosity	l	258-323	0.5-2	--	--	2%	comp	
Higashi; Iwaki Meisei U.; Japan V-L-E correlation	s1,sv	230-T <sub>c</sub>	-	--	--	--	comp	[Hg89]
critical region correlation	-	-	-	--	-	-	comp	[Hg89a]
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	253-338	-	0-100	158	0.3%	comp	[Kb90a]
Gorenflo; U. Paderborn; FRG vapor pressure	l-v	293-T <sub>c</sub>	-	0-89	95	0.2%	comp	[Rt89]
sat. liquid density	s1	293-T <sub>c</sub>	-	0-89	95	0.2%	comp	[Rt89]
sat. vapor density	sv	293-T <sub>c</sub>	-	0-89	95	0.8%	comp	[Rt89]
critical parameters	-	-	-	0-89	9	--	comp	[Rt89]
Sami; U. Moncton; Canada heat capacity	l,v	283-353	0.5-1.4	-	-	2%	in prog	
LaRue; CRIQ; Canada bubble point pressure	l-v	.65-.85 T <sub>c</sub>	-	0-100	-	1%	comp	[Lr90]
R22/123 Schramm; Phys. Chem. Inst.; FRG second virial coefficient	v	268-296	-	--	2	3%	comp	
R134a/152a Baehr; U. Hannover; FRG vapor-liquid equilibria	l-v	300-373	-	25-75	40	0.1%	7/89-6/91	
P-V-T-x	l,v	293-433	0.1-16	25-75	500	0.1%	7/89-6/91	
Tamatsu; Keio U.; Japan vapor-liquid equilibria	l-v	300-T <sub>c</sub>	-	20-80	--	0.1%	8/90-->	
P-V-T-x	l,v	300-443	0.5-10	20-80	--	0.1%	8/90-->	
Holste; Texas A&M U.; USA vapor-liquid equilibria	l-v	180-T <sub>c</sub>	-	50	--	0.1%	1/91-6/91	
P-V-T-x	l,v	180-400	0-70	50	--	0.1%	1/91-6/91	
Bier; U. Karlsruhe; FRG vapor pressure	l-v	203-T <sub>c</sub>	-	0-100	-	0.1%	comp	[Bi90]
critical parameters	-	-	-	-	-	-	comp	[Bi90]
Oellrich; U. Karlsruhe; FRG equation of state	l,v	-	-	-	-	-	?/89-?/92	
Morrison; NIST; USA bubble point pressure	l-v	268-T <sub>c</sub>	-	50	10	-	comp	

### Mixture Studies (continued)

Mixture/Investigator/ /Property	phase	T (K)	range of data p (MPa)	x	no. points	est. accuracy	start/end dates	note /ref.
R134a/134								
Morrison; NIST; USA bubble point pressure	l-v	268-T <sub>c</sub>	-	50	10	-	comp	
R134a/123								
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	288-333	-	--	--	0.1%	?/89-->	
Nakaiwa; Nat. Chem. Lab; Japan equation of state	--	313-363	0.2-3.2	--	--	--	comp	[Nk90]
R134a/141b								
Kubota; Kobe U.; Japan vapor-liquid equilibria	l-v	278-333	-	--	76	0.1%	comp	[Kb90]
R152a/134								
Maezawa; Keio U.; Japan bubble point pressure	l-v	280-380	-	20-80	44	20kPa	comp	[Mz91]
saturated liquid density	s <sub>l</sub>	280-380	-	20-80	44	0.2%	comp	[Mz91]
vapor-liquid equilibria	l-v	280-380	-	20-80	44	0.1%	comp	[Mz91]
Morrison; NIST; USA bubble point pressure	l-v	268-383	-	50	10	-	comp	
R152a/142b								
Maezawa; Keio U.; Japan bubble point pressure	l-v	280-400	-	20-80	48	20kPa	comp	[Mz90a]
saturated liquid density	s <sub>l</sub>	280-400	-	20-80	48	0.2%	comp	[Mz90a]
vapor-liquid equilibria	l-v	280-400	-	20-80	48	0.1%	comp	[Mz90a]
R152a/114								
Higashi; Iwaki Meisei U.; Japan V-L-E correlation	s <sub>l</sub> ,s <sub>v</sub>	230-T <sub>c</sub>	-	--	--	--	comp	[Hg89]
R227/123								
Gorenflo; U. Paderborn; FRG bubble-point pressure	l-v	293-423	-	(3 comp)	--	--	9/90-->	
saturated liquid density	s <sub>l</sub>	293-423	-	(3 comp)	--	--	9/90-->	
saturated vapor density	s <sub>v</sub>	293-423	-	(3 comp)	--	--	9/90-->	

## Mixture Studies (continued)

### Notes and References

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- [Mz90c] Y. Maezawa, to be published in Fluid Phase Equilibria (1990).
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other researcher:

R. K. Malhotra

apparatus and techniques employed:

pressure-volume-temperature:

viscosity:

sample purity analysis:

bellows volumometer; vibrating tube densimeter

not specified

supplier's analysis

## CANADA

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apparatus and techniques employed:

vapor-liquid equilibria

variable volume cell

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CANADA (continued)

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apparatus and techniques employed:

viscosity                              falling ball viscometer

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apparatus and techniques employed:  
thermal conductivity/diffusivity

transient hot wire

PEOPLE'S REPUBLIC OF CHINA

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techniques employed:

equation of state:

Redlich-Kwong-Soave and Martin-Hou equations

Tsinghua University  
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Han Li-Zhong

apparatus and techniques employed:

vapor pressure:

saturation density:

pressure-volume-temperature:

sound speed:

surface tension:

thermal conductivity:

viscosity:

sample purity analysis:

constant volume method

magnetic suspension densimeter

Burnett method

acoustic method

capillary rise method

steady-state method

capillary method

supplier's analysis

PEOPLE'S REPUBLIC OF CHINA (continued)

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**apparatus and techniques employed:**

vapor pressure: constant volume method  
saturation density: not specified  
critical parameters: observation of meniscus for temperature and density  
sample purity analysis: not specified

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**Laboratory of Chemical Engineering Thermodynamics**  
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**apparatus and techniques employed:**

mixture V-L-E: Rose-William cell; vapor circulation technique; Martin-Hou  
equation of state  
sample purity analysis: own analysis

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apparatus and techniques employed

pressure-volume-temperature:  
sample purity analysis:

constant volume piesometer  
own analysis

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other researchers:

apparatus and techniques employed

vapor pressure:

not specified

pressure-volume-temperature:

vibrating tube densimeter

critical parameters:

not specified

sound speed:

not specified

thermal conductivity:

coaxial cylinder

sample purity analysis:

supplier's analysis

FEDERAL REPUBLIC OF GERMANY

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U. Delfs

apparatus and techniques employed  
ideal gas properties: statistical thermodynamics

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apparatus and techniques employed  
sound speed: photon correlation spectroscopy  
thermal diffusivity: photon correlation spectroscopy  
sample purity analysis: not specified

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apparatus and techniques employed  
vapor pressure: not specified  
saturated liquid density: pycnometer  
viscosity: falling ball viscometer  
sample purity analysis: own analysis  
predictive methods: functional group methods

FEDERAL REPUBLIC OF GERMANY (continued)

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apparatus and techniques employed

vapor pressure:

not specified

saturated liquid density:

vibrating tube densimeter

pressure-volume-temperature:

Burnett apparatus; vibrating tube densimeter

mixture V-L-E

VLE apparatus

sample purity analysis:

own analysis

Universität Gesamthochschule Paderborn  
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apparatus and techniques employed

vapor pressure:

static equilibrium cell

saturation density:

static equilibrium cell with vibrating tube densimeter

sample purity analysis:

own analysis

Universität Kaiserslautern  
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apparatus and techniques employed

equation of state:

Bender equation of state

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apparatus and techniques employed  
dielectric constant: capacitance technique

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apparatus and techniques employed  
vapor pressure: static equilibrium cell  
pressure-volume-temperature: Burnett apparatus  
critical parameters: static equilibrium cell  
heat capacity: adiabatic flow calorimeter  
sample purity analysis: own analysis & supplier's analysis  
equation of state: not specified

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apparatus and techniques employed  
pressure-volume-temperature: not specified  
critical parameters: not specified  
surface tension: capillary rise  
thermal diffusivity: dynamic light scattering  
refractive index: not specified  
viscosity: oscillating disk viscometer  
sample purity analysis: supplier's analysis

FEDERAL REPUBLIC OF GERMANY (continued)

Physikalisch-Chemisches Institut der Universität  
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apparatus and techniques employed  
pressure-volume-temperature:  
sample purity analysis: measurement of second virial coefficients  
supplier's analysis

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apparatus and techniques employed  
vapor pressure: constant volume method  
pressure-volume-temperature: constant volume method  
triple point temperature: not specified  
thermal conductivity: guarded hot plate  
sample purity analysis: supplier's analysis

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apparatus and techniques employed  
dielectric constant: cyclic expansion method  
sample purity analysis: own analysis

FEDERAL REPUBLIC OF GERMANY (continued)

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Postfach 10 21 48  
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other researchers:

apparatus and techniques employed

vapor pressure: single- and dual-sinker densimeters  
saturated liquid density: single- and dual-sinker densimeters  
saturated vapor density: single- and dual-sinker densimeters  
pressure-volume-temperature: single- and dual-sinker densimeters  
sample purity analysis: supplier's analysis  
equation of state: multi-property fit

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apparatus and techniques employed

vapor pressure: isochoric PVT  
pressure-volume-temperature: isochoric PVT; Burnett apparatus  
sound speed spherical resonator  
sample purity analysis: own analysis

FEDERAL REPUBLIC OF GERMANY (continued)

Ruhr Universität Bochum  
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apparatus and techniques employed

thermal diffusivity: photon correlation spectroscopy  
sample purity analysis: supplier's analysis

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apparatus and techniques employed

thermal conductivity: transient hot wire  
sample purity analysis: supplier's analysis  
data base project

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apparatus and techniques employed

thermal conductivity: transient hot wire  
sample purity analysis: not specified

FEDERAL REPUBLIC OF GERMANY (continued)

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Dr. J. Senst

apparatus and techniques employed  
equation of state: Redlich-Kwong-Soave equation; incremental methods  
(Lydersen, Riedel, Westmeier, etc.)

## GREECE

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other researchers:  
Mr. L. Karagiannidis

apparatus and techniques employed:  
thermal conductivity:                    transient hot wire  
viscosity:                                vibrating wire  
sample purity analysis:                not specified

## INDIA

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Instrumentation and Services Unit  
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technique employed:  
equation of state:                      corresponding states

**ITALY**

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**apparatus and techniques employed**

vapor pressure:                    constant volume technique  
pressure-volume-temperature:    constant volume technique  
sample purity analysis:            own analysis

JAPAN

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10, Goikaigan, Ichihara-shi, Chiba 290

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apparatus and techniques employed:

vapor pressure:

saturation density:

pressure-volume-temperature:

critical parameters:

sample purity analysis:

constant volume method

buoy method; constant volume method

constant volume method

visual observation of meniscus for density and temperature

own analysis

Iwaki Meisei University  
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apparatus and techniques employed

surface tension:

mixture V-L-E:

Wilhelmy method

original correlation

Kanagawa Institute of Technology  
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apparatus and techniques employed

vapor pressure:

saturation density:

pressure-volume-temperature

equation of state:

constant volume method

buoy method; constant volume method

constant volume method

extended Benedict-Webb-Rubin

JAPAN (continued)

Keio University  
Thermodynamics Laboratory  
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apparatus and techniques employed

vapor pressure:

magnetic densimeter; constant volume method; Burnett method

saturated liquid density:

magnetic densimeter; visual critical point cell; constant volume method

saturated vapor density:

visual critical point cell

pressure-volume-temperature:

magnetic densimeter; constant volume method; Burnett-isochoric method

critical parameters:

visual cell for temperature and density

heat capacity:

flow calorimeter

sample purity analysis:

supplier's analysis

equation of state:

25-term virial

Keio University  
3-14-1, Hiyoshi, Kohoku-ku, Yokohama 223

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apparatus and techniques employed

thermal conductivity:

transient hot wire

viscosity:

capillary viscometer

sample purity analysis:

supplier's analysis

JAPAN (continued)

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apparatus and techniques employed

vapor pressure:  
pressure-volume-temperature

constant volume method  
vibrating-tube densimeters (commercial and modified);  
constant volume method; Burnett method; high-pressure

Burnett method

observation of meniscus

flow calorimeter

vapor liquid circulation method

frequency counting method; LCR meter

stationary coaxial cylinder; transient hot wire

rolling ball viscometer; falling cylinder viscometer

supplier's analysis

critical parameters:

heat capacity:

mixture V-L-E

dielectric constant:

thermal conductivity:

viscosity:

sample purity analysis:

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apparatus and techniques employed

sound speed:

sing-around method

thermal conductivity:

transient hot wire

sample purity analysis:

supplier's analysis

JAPAN (continued)

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apparatus and techniques employed  
mixture V-L-E static V-L-E method  
sample purity analysis: supplier's analysis

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apparatus and techniques employed  
surface tension: single and differential capillary rise  
sample purity analysis: supplier's analysis

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mixture V-L-E: not specified  
sample purity analysis: own analysis

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apparatus and techniques employed

vapor pressure:                static method  
pressure-volume-temperature: isochoric method  
saturated liquid density:    pycnometer  
viscosity:                    oscillating-disk viscometer; capillary viscometer  
sample purity analysis:      supplier's analysis

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techniques employed:  
equation of state:

Carnahan-Starling equation

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apparatus and techniques employed:  
surface tension:  
refractive index:  
thermal conductivity:  
sample purity analysis:

capillary rise technique  
optical method  
transient hot wire  
supplier's analysis

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thermal conductivity:  
sample purity analysis:  
equation of state:

transient hot wire  
supplier's analysis  
not specified

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**apparatus and techniques employed**

pressure-volume-temperature:  
dielectric constant:  
thermal conductivity:  
sample purity analysis:

vibrating tube densimeter  
capacitance measurement  
concentric cylinder method; transient hot wire  
supplier's analysis

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**apparatus and techniques employed**

vapor pressure:  
saturated liquid density:  
heat capacity:  
refractive index:  
sample purity analysis:

not specified  
not specified  
not specified  
not specified  
not specified

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**apparatus and techniques employed**

pressure-volume-temperature:         vibrating tube densimeter  
heat capacity:                          Setaram BT calorimeter  
mixture V-L-E                         Jones circulation unit  
viscosity:                               Höppler viscometer  
sample purity analysis:               supplier's analysis

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**techniques employed:**

equation of state:                      virial equation

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apparatus and techniques employed

enthalpy:                              flow calorimeter  
sample purity analysis:                supplier's analysis

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apparatus and techniques employed

sound speed:                            spherical resonator  
thermal conductivity                  transient hot wire  
viscosity                                vibrating wire  
sample purity analysis:                supplier's analysis  
equation of state:                     Wagner algorithm

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apparatus and techniques employed

pressure-volume-temperature:	single sinker magnetic suspension densimeter
thermal conductivity:	transient hot wire
sample purity analysis:	supplier's analysis

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apparatus and techniques employed

viscosity:	gas phase capillary flow viscometry
sample purity analysis:	not specified

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apparatus and techniques employed  
vapor pressure: not specified  
critical parameters: not specified  
sample purity analysis: own analysis

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apparatus and techniques employed  
pressure-volume-temperature: gas expansion technique  
speed of sound: pulse-echo-overlap technique  
sample purity analysis: supplier's analysis

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apparatus and techniques employed  
equation of state: fundamental EOS, MBWR, selection algorithm

UNITED STATES (continued)

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apparatus and techniques employed

equation of state:                        renormalization theory for critical region

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apparatus and techniques employed

vapor pressure:

isochoric apparatus; V-L-E apparatus  
isochoric apparatus; V-L-E apparatus; magnetic suspension  
densimeter

saturated liquid density:

isochoric apparatus; V-L-E apparatus

saturated vapor density:

isochoric apparatus; magnetic suspension densimeter;  
vibrating tube densimeter

pressure-volume-temperature:

adiabatic isochoric calorimeter

heat capacity:

transient hot wire

thermal conductivity:

torsionally oscillating quartz crystal

viscosity:

gas chromatography/mass spectrometry; infrared and  
ultraviolet spectrometry; Karl Fisher moisture analysis

sample purity analysis:

Jacobsen-Stewart BWR; Schmidt-Wagner; extended  
corresponding states; Carnahan-Starling-DeSantis

equation of state:

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apparatus and techniques employed

vapor pressure:

variable volume cell; Burnett-isochoric apparatus;  
ebulliometer

saturated liquid density:

variable volume cell; vibrating-tube densimeter; visual cell  
variable volume cell; Burnett-isochoric apparatus; vibrating  
tube densimeter

pressure-volume-temperature:

Burnett-isochoric apparatus; vibrating-tube densimeter

critical parameters:

visual cell; variable volume cell

sound speed:

spherical acoustic resonator

surface tension:

differential capillary rise technique

dielectric constant:

capacitance technique

sample purity analysis:

NIST-Boulder

equation of state:

Carnahan-Starling-DeSantis

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apparatus and techniques employed:

equation of state:

Lee-Kessler-Plöcker

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apparatus and techniques employed

vapor pressure: isochoric apparatus  
saturated liquid density: vibrating tube densimeter  
pressure-volume-temperature: vibrating tube densimeter; isochoric apparatus  
critical parameters: visual cell  
sample purity analysis: capillary gas-liquid chromatography

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apparatus and techniques employed

vapor pressure: isochoric apparatus  
pressure-volume-temperature: isochoric apparatus; Burnett apparatus; continuously  
weighed pycnometer; vibrating tube densimeter  
critical parameters: visual cell  
sample purity analysis: supplier's analysis

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apparatus and techniques employed

ideal gas properties: statistical mechanics  
fluid property database: wide variety of compounds including refrigerants





## BIBLIOGRAPHIC DATA SHEET

1. PUBLICATION OR REPORT NUMBER	NISTIR 3969
2. PERFORMING ORGANIZATION REPORT NUMBER	
3. PUBLICATION DATE	June 1991

## 4. TITLE AND SUBTITLE

A Survey of Current Worldwide Research on the Thermophysical Properties of Alternative Refrigerants

## 5. AUTHOR(S)

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## 6. PERFORMING ORGANIZATION (IF JOINT OR OTHER THAN NIST, SEE INSTRUCTIONS)

U.S. DEPARTMENT OF COMMERCE  
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## 7. CONTRACT/GANT NUMBER

## 8. TYPE OF REPORT AND PERIOD COVERED

## 9. SPONSORING ORGANIZATION NAME AND COMPLETE ADDRESS (STREET, CITY, STATE, ZIP)

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## 10. SUPPLEMENTARY NOTES

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## 11. ABSTRACT (A 200-WORD OR LESS FACTUAL SUMMARY OF MOST SIGNIFICANT INFORMATION. IF DOCUMENT INCLUDES A SIGNIFICANT BIBLIOGRAPHY OR LITERATURE SURVEY, MENTION IT HERE.)

This survey represents an exhaustive compilation of the research activities throughout the world concerned with either measurements or correlations of the thermophysical properties of alternative refrigerants. The properties covered in this study include thermodynamic, transport, phase equilibria, and other properties such as dielectric constant and refractive index. This survey has included a wide range of fluids (including R23, R32, R125, R143a, R22, R134a, R152a, R134, R124, R142b, R123, R123a, R141b) along with mixtures containing at least one of these fluids. This report presents in tabular form summary information about each research activity; this survey does not present raw data or correlating equations.

## 12. KEY WORDS (6 TO 12 ENTRIES; ALPHABETICAL ORDER; CAPITALIZE ONLY PROPER NAMES; AND SEPARATE KEY WORDS BY SEMICOLONS)

hydrochlorofluorocarbons; hydrofluorocarbons; refrigerants; survey; thermodynamic properties; thermophysical properties; transport properties

## 13. AVAILABILITY

X
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ORDER FROM SUPERINTENDENT OF DOCUMENTS, U.S. GOVERNMENT PRINTING OFFICE, WASHINGTON, DC 20402.
X ORDER FROM NATIONAL TECHNICAL INFORMATION SERVICE (NTIS), SPRINGFIELD, VA 22161.

\*U.S. GOVERNMENT PRINTING OFFICE 1991-0-576-343/45150

## 14. NUMBER OF PRINTED PAGES

80

## 15. PRICE



